Cyberinfrastructure-enabled Molecular Products Design and Engineering: Challenges and Opportunities

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## Outline

Molecular Products Design Data, Information and Knowledge Modeling Challenges **Cyberinfrastructure** Ontological Informatics Industrial Case Studies Lubrizol: Fuel Additives Design Caterpillar: Rubber Products Design ExxonMobil: Catalyst Design Eli Lilly: Seromycin Formulation for MDR-TB Summary



Venkat Venkatasubramanian, Keynote Lecture, European Congress in Chem. Engg, Copenhagen, Sept 2007

## Acknowledgements Materials Design

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- DOE
- Indiana 21<sup>st</sup> Century Research and Technology Fund
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LIPS

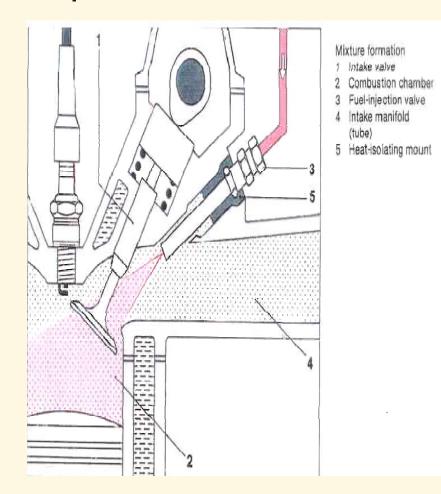
Abbott



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## LUBRIZOL: Fuel Additive Design

.



- EPA requirement: Minimize intake-valve deposits (IVD)
- Approach: Fuel Additives

#### Performance measure

- BMW Test for IVD
- Stipulated to be less than 100 mg over a 10,000 mile road test

## Expensive and time-consuming testing

Around \$8000 for a single datum

 Problem: Design fuel-additives that meet desired IVD performance levels

#### **Intake Valve and Manifold**



### CATERPILLAR



About 1000 Rubber Parts in Failure Critical Functions

Tires, Treads, Hoses, Shock Absorbers, Orings, Gaskets, Mounts ...

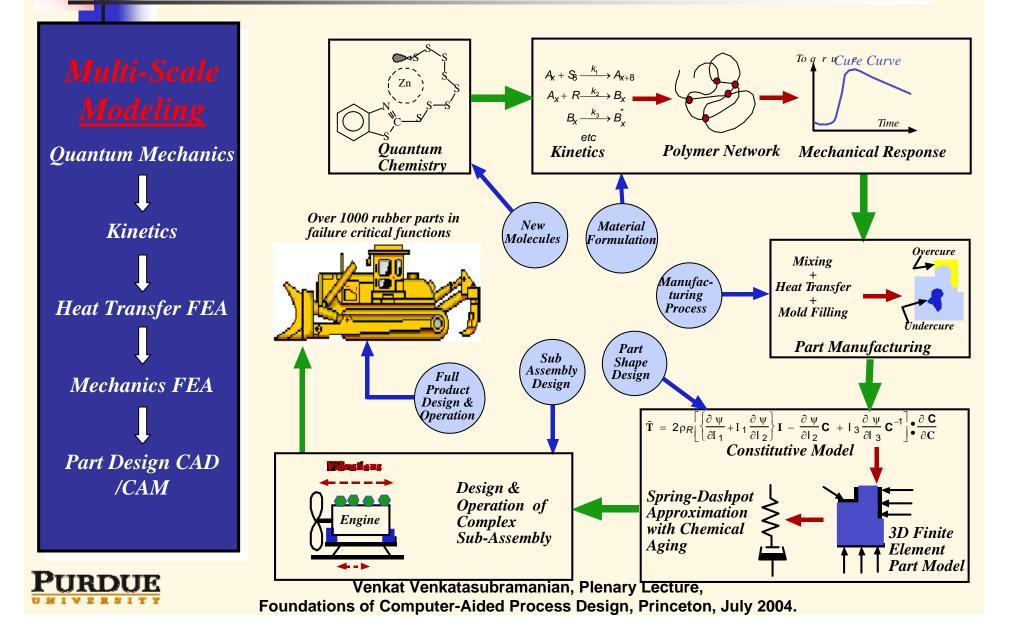
Reliability and Warranty Problems



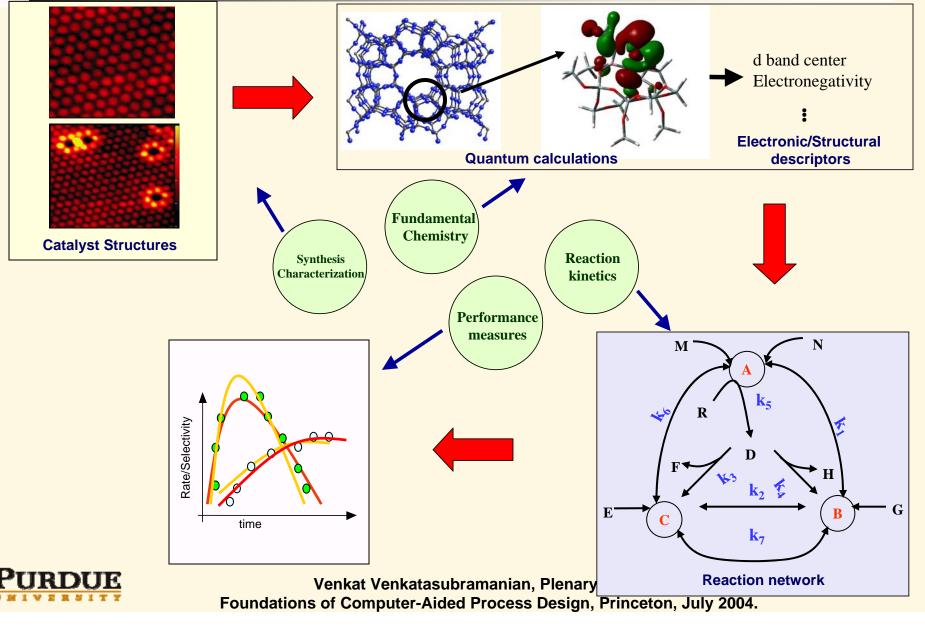




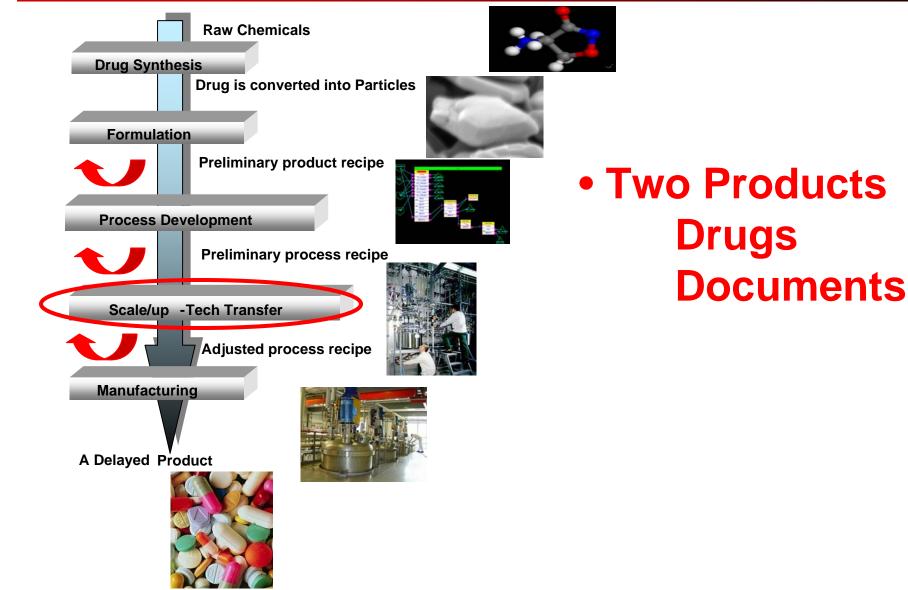
### Caterpillar's Multi-Scale Modeling Challenge: Design of Formulated Rubber Parts



### ExxonMobil's Grand Challenge: Catalyst Design via Combinatorial Chemistry



### **Pharmaceutical Product Development and Engineering**



## **Molecular Products Design**

- Given a set of desired performance specifications, how does one rationally and efficiently identify the optimal product structures and formulations?
- \$200+ Billion/yr industry: Major Opportunity for ChEs
- Areas of Application
  - Engineering Materials
    - Fuel and Oil Additives
    - Polymer Composites
    - Rubber Compounds
    - Catalysts
    - Solvents, Paints and Varnishes.....
  - Pharmaceuticals
    - Drug Design
  - Agricultural Chemicals
    - Pesticides
    - Insecticides



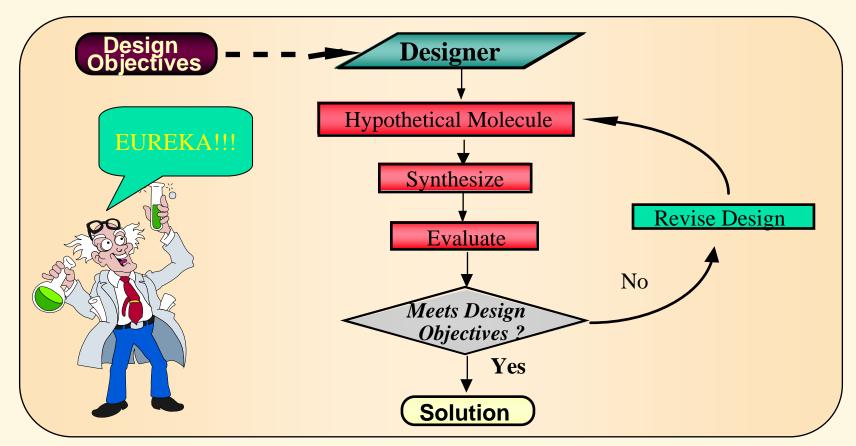


## Different Products, But Common Challenges

- Lots of Data
- Uncertain/Noisy Data
- Complex chemistry, lots of species
- Nonlinear systems and processes
- Incomplete, Uncertain, Mechanisms
- Combinatorially large search spaces
- Need Multi-scale Models
- Hundreds of Differential and Algebraic Equations to formulate and solve
- Laborious and time consuming model development process
- Limited human expertise







**Drawback: Protracted and Expensive Design Cycle** 

Need a Rational, Automated Approach: Discovery Informatics



# Need a New Paradigm Cyberinfrastructure Methods and Tools

## Ontology-based Discovery Informatics

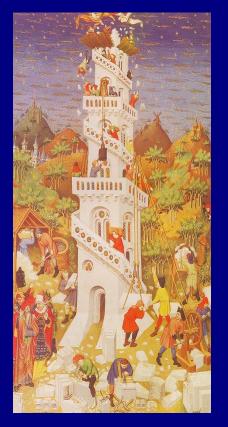


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## Data, Information, and Knowledge

Data What's going on? Raw, does not inform much Information How are the variables related? Correlations and relationships Knowledge Why are they related? Develop Mechanistic understanding First-Principles Based Math Models Heuristics



Tower of Babel of Data, Information and Models



Venkat Venkatasubramanian, Plenary Lecture, Chemical Process Control 7, Canada, Jan 2006

## What is an Ontology?

- Originated in Philosophy
  - Study of Existence
  - Not to be confused with Epistemology: Theory of Knowledge and Knowing
- **Computer Science and Artificial Intelligence** 
  - A formal, explicit specification of a shared conceptualization
  - Knowledge representation in AI
    - Logic, Semantic Networks, Frames, Objects, Ontology
  - Web-driven development
- Semantic Richness: Description Logic (DL) provides foundation for formal reasoning
- Easily create, share and reuse knowledge
- Semantic Search



Venkat Venkatasubramanian, Plenary Lecture, Pharmaceutical Sciences World Congress, Amsterdam, April 2007

## **Based on Set Theory and First-order Logic**

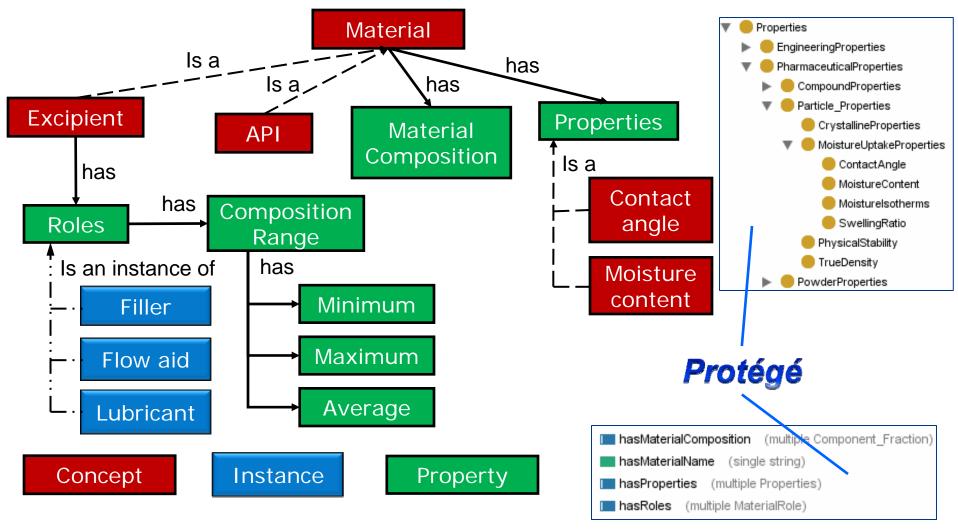
An ontology is a 5-tuple  $O := (C, R, H^c, rel, A^o)$  consisting of

- Two disjoint sets *C* and *R* whose elements are called concept identifiers and relation identifiers, respectively
- A concept hierarchy  $H^C$ :  $H^C$  is a directed, transitive relation  $H^C \subseteq C \times C$  which is called concept hierarchy or taxonomy.  $H^C(C_1, C_2)$  means that  $C_1$  is a subconcept of  $C_2$ .
- A function  $rel: R \to C \times C$  that relates concepts non-taxonomically. The function dom:  $R \to C$  with  $dom(R) \coloneqq \Pi_1(rel(R))$  gives the domain of R, and range:  $R \to C$  with  $range(R) \coloneqq \Pi_2(rel(R))$  give its range. For  $rel(R) = (C_1, C_2)$  we also write  $R(C_1, C_2)$ .
- A set of axioms A<sup>o</sup>, expressed in an appropriate logic language, e.g. first order logic



Venkat Venkatasubramanian, Plenary Lecture, Pharmaceutical Sciences World Congress, Amsterdam, Apr 2007

## **Ontology: A Simple Example**



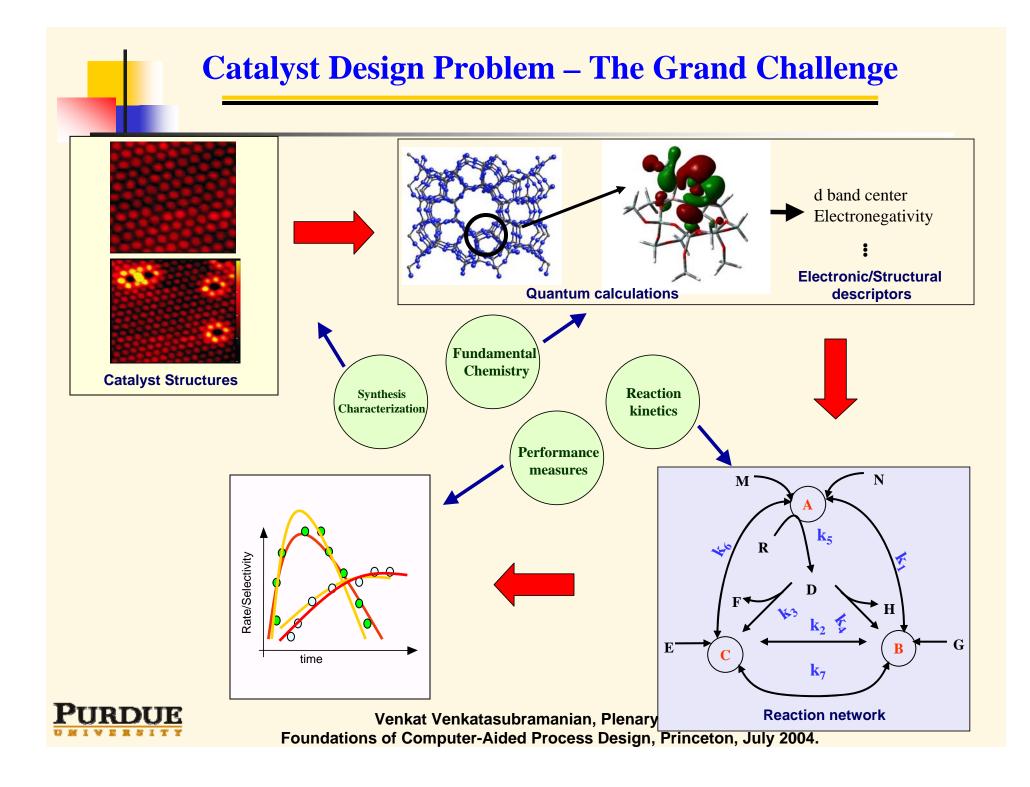


STRUCTURED ORGANIC PARTICULATE SYSTEMS RUTGERS UNIVERSITY PURDUE UNIVERSITY NEW JERSEY INSTITUTE OF TECHNOLOGY UNIVERSITY OF PUERTO RICO AT MAYAGÜEZ

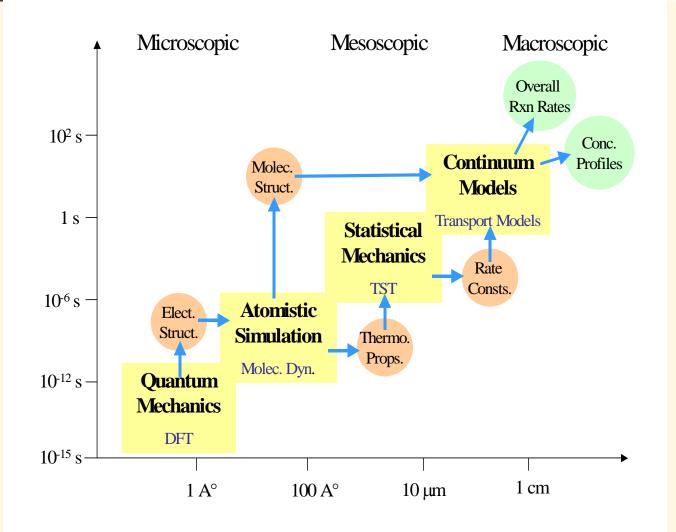
ENGINEERING RESEARCH CENTER FOR



### Web Ontology Language: OWL



#### **Modeling at different Length and Time Scales**



PURDUE

## Paraffin Aromatization

- Identify a catalyst formulation for light paraffin aromatization that is superior to Ga/H-ZSM-5 in terms of:
  - Higher Benzene, Toluene, Xylene (B/T/X) selectivity
  - Higher Hydrogen selectivity
- Microkinetic model development for the kinetic description of the system



### **Previous Work**

#### Microkinetic Analysis (Dumesic, 1993)

First unified view of reaction engineering on catalytic surfaces

Incomplete forward problem

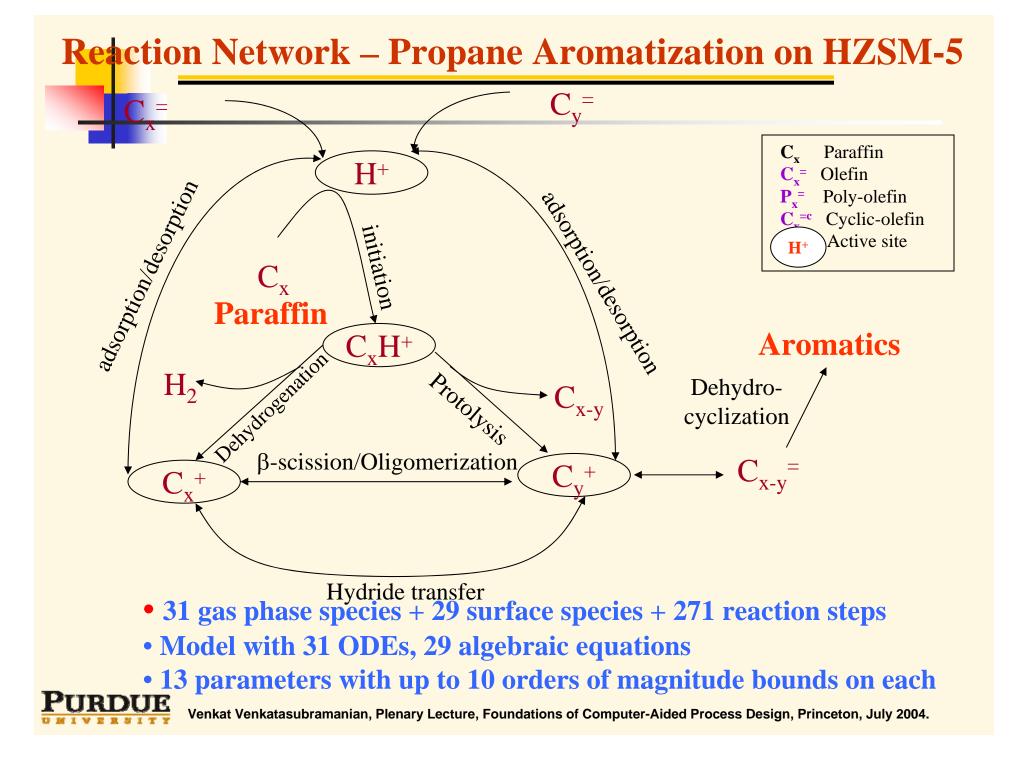
Lacks clear view of the design perspective (inverse problem)

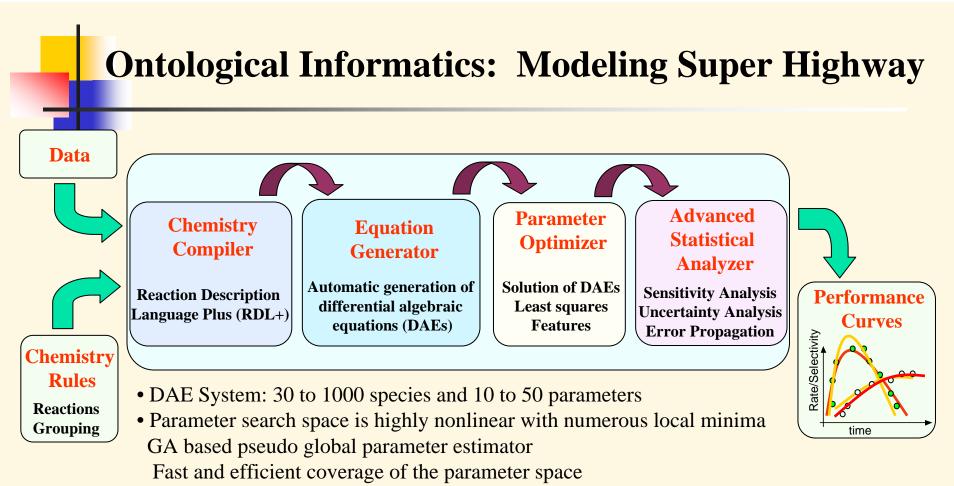
#### Empirical Catalyst Design (Baerns, 2000)

First attempt to "design" catalysts Completely based on "guided" experiments – time consuming and expensive No fundamental understanding of the system (forward problem)

Ertl, Rasmussen, Lauterbach: Surface Science Studies Steve Jaffe: Composition based modeling of large systems Jens Norskov: Computation based studies Symyx, Novodynamics, Lauterbach: Combinatorial HTE





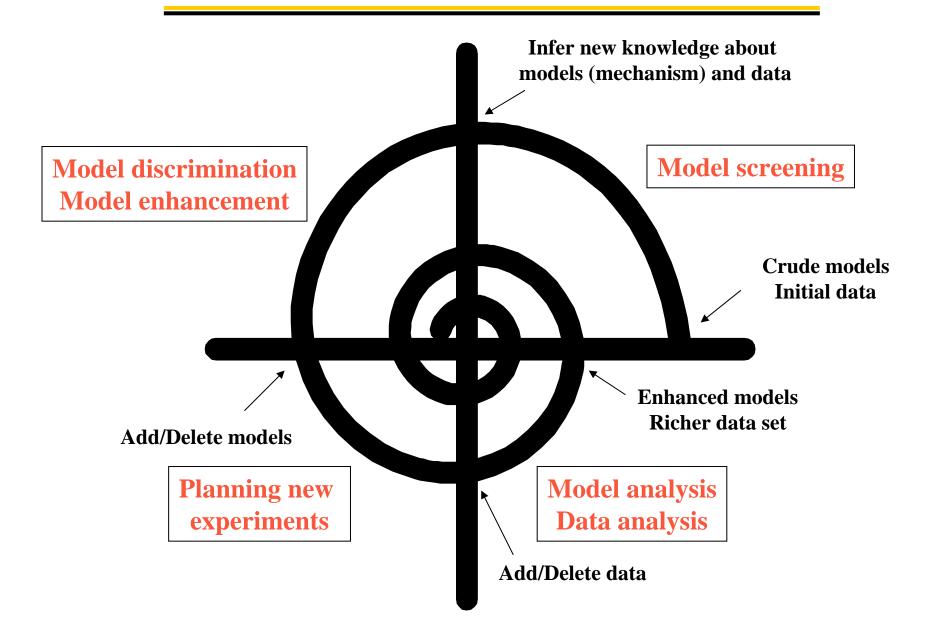


- Optimization: Traditional least-squares and features-based objectives
- J.M. Caruthers, J.A. Lauterbach, K.T. Thomson, V. Venkatasubramanian, C.M. Snively, A. Bhan, S. Katare and G. Oskarsdottir, "Catalyst Design: Knowledge Extraction from High Throughput Experimentation", In "Understanding Catalysis from a Fundamental Perspective: Past, Present, and Future", A. Bell, M. Che and W.N. Delgass, Eds., Invited Paper for the 40th Anniversary Issue of the *Journal of Catalysis*, 2003.

Katare, S., Caruthers, J. M., Delgass, W. N., Venkatasubramanian, V., "An Intelligent System for Reaction Kinetic Modeling and Catalyst Design", *Ind. Eng. Chem. Res. and Dev.*, 2004.



#### **Model Refinement Procedure**

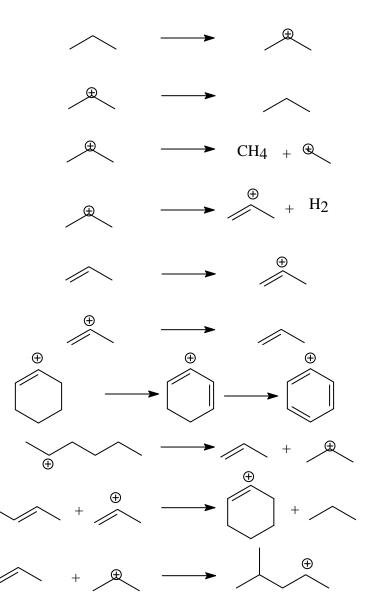


#### **Chemistry Rules for Propane Aromatization on HZSM-5**

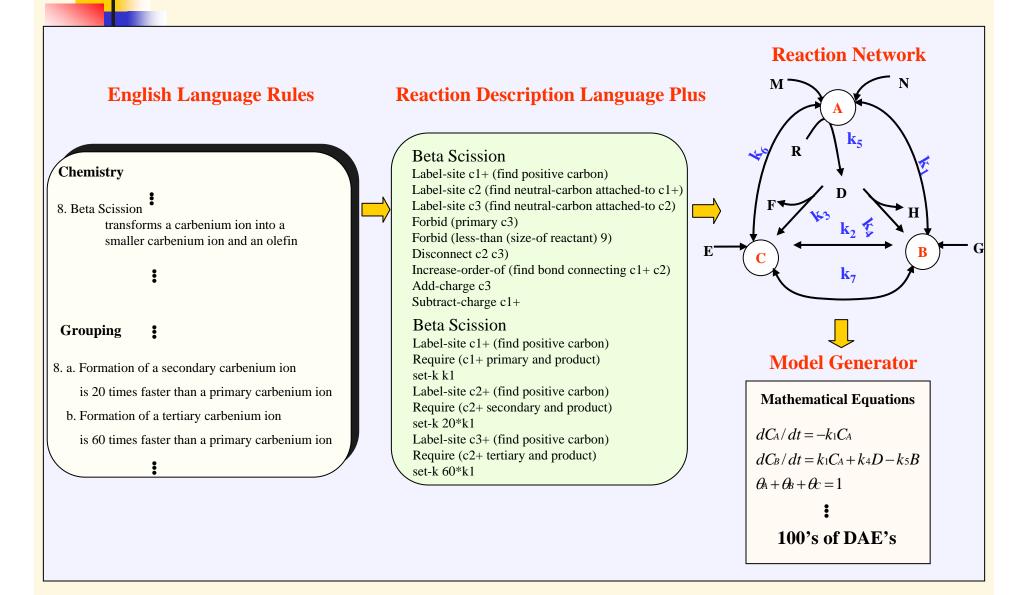
### **Chemistry Rules**

- 1. Alkane adsorption
- 2. Alkane desorption
- **3.** Carbonium ion protolysis
- 4. Carbonium ion dehydrogenation
- 5. Olefin adsorption
- 6. Olefin desorption
- 7. Aromatization
- 8. Beta-Scission
- 9. Hydride Transfer
- **10. Oligomerization**

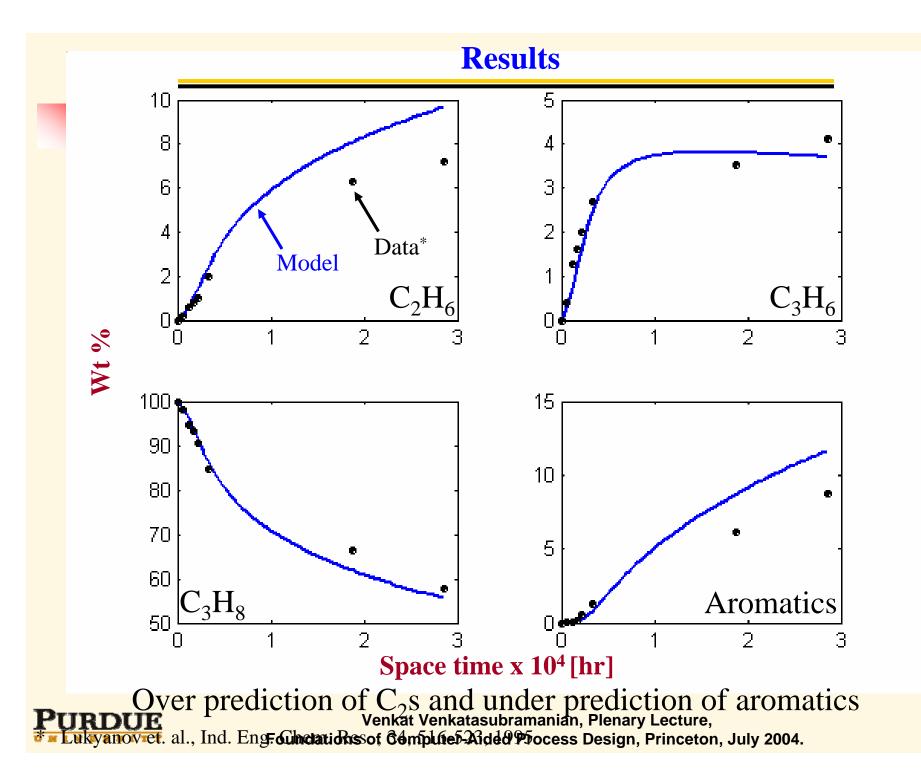
#### **Representative Chemical Reactions**

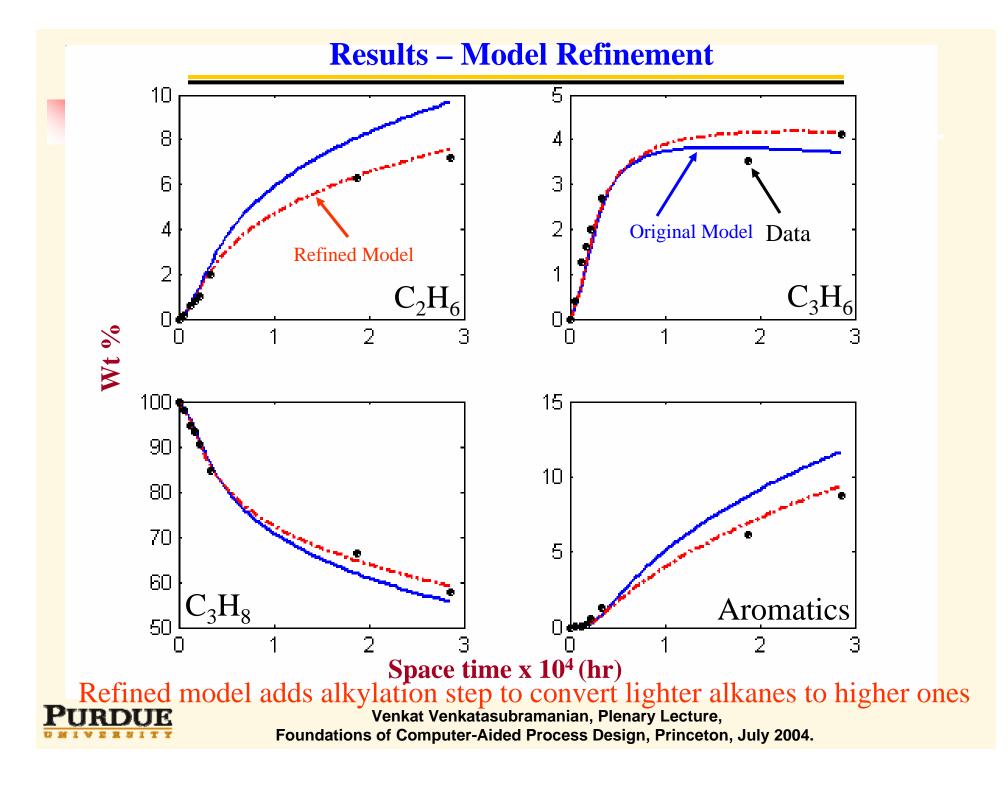


### **Modeling Super Highway: Reaction Modeling Suite (RMS)**









### **GA Based Pseudo Global Parameter Estimator**

**Performance comparison on test problems – worst case: 3 ODEs/5 parameters** 

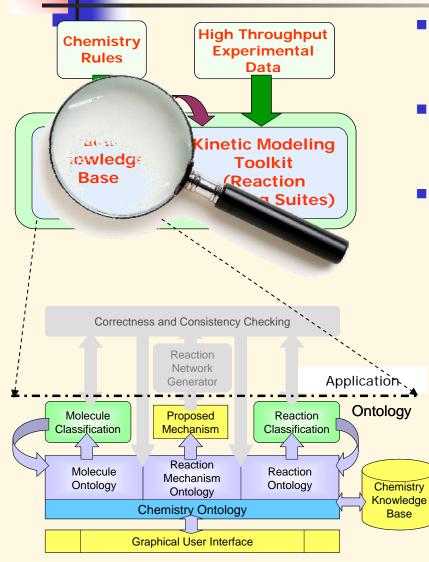
S.no.	Name	Esposito & Floudas (2000) Global optimizer			GA based procedure			
		υ	Objective	CPU s reported min max	υ	Objective	Time taken (CPU s)	Scaled CPU s Time taken *671/211 (% Saving)
1	First order irreversible chain reaction	5.0035 1.0000	1.18584x10 <sup>-6</sup>	2.92 20.05	5.0122 0.9976	9.25418x10 <sup>-6</sup>	0.24	0.76 ( <b>74</b> )
2a	First order reversible chain reaction	4.0000 2.0000 40.013 20.007	1.8897x10 <sup>-7</sup>	568.44 6164.3	3.9813 1.9759 39.787 19.887	8.1313x10 <sup>-6</sup>	0.45	1.43 ( <b>100</b> )
2b	Same as 2a but with error in data	4.021 2.052 39.45 19.62	1.586x10 <sup>-3</sup>	272.91 1899.82	4.001 2.027 39.22 19.50	1.589x10 <sup>-3</sup>	0.5	1.59 ( <b>99</b> )
3	Catalytic cracking of gas oil	12.214 7.9798 2.2216	2.65567x10 <sup>-3</sup>	79.77 1185	12.246 7.9614 2.2351	2.68017x10 <sup>-3</sup>	0.38	1.21 ( <b>98</b> )
4	Bellman's problem	4.5704x10 <sup>-6</sup> 2.7845x10 <sup>-4</sup>	22.03094	36.16 12222	4.5815x10 <sup>-6</sup> 2.7899x10 <sup>-4</sup>	22.2885	3.54	11.26 ( <b>69</b> )
5	Methanol-to- hydrocarbon process	5.1981 1.2112 0 0 0	0.10652	1361.8 19125	$\begin{array}{r} 5.2212 \\ 1.2320 \\ 1.6363 x 10^{-31} \\ 4.0059 x 10^{-12} \\ 0.004665 \end{array}$	0.10586	2.08	6.61 ( <b>100</b> )
6	Lotka-Volterra Problem	3.2434 0.9209	1.24924x10 <sup>-3</sup>	367.26 9689.67	3.1434 0.9583	2.39784x10 <sup>-3</sup>	0.56	1.78 ( <b>100</b> )

**Our zeolite model** 

31 ODEs, 29 Algebraic equations 13 parameters 9 concentration curves Reasonable comparison to experimental data

2 hours on a Sun 400 MHz solaris machine

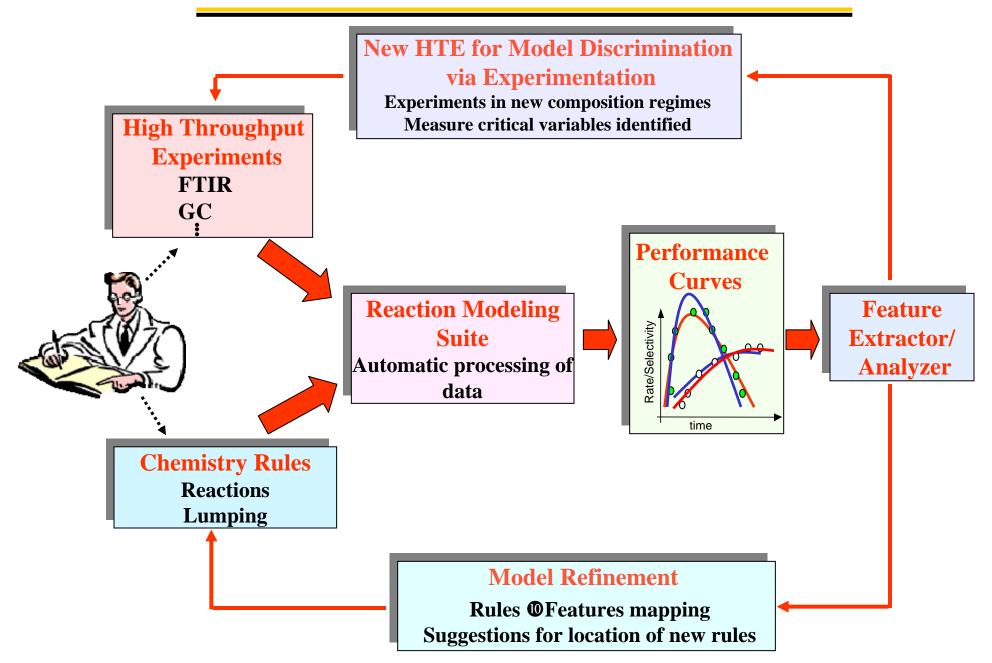
### Ontological Informatics for Catalyst Design: Summary



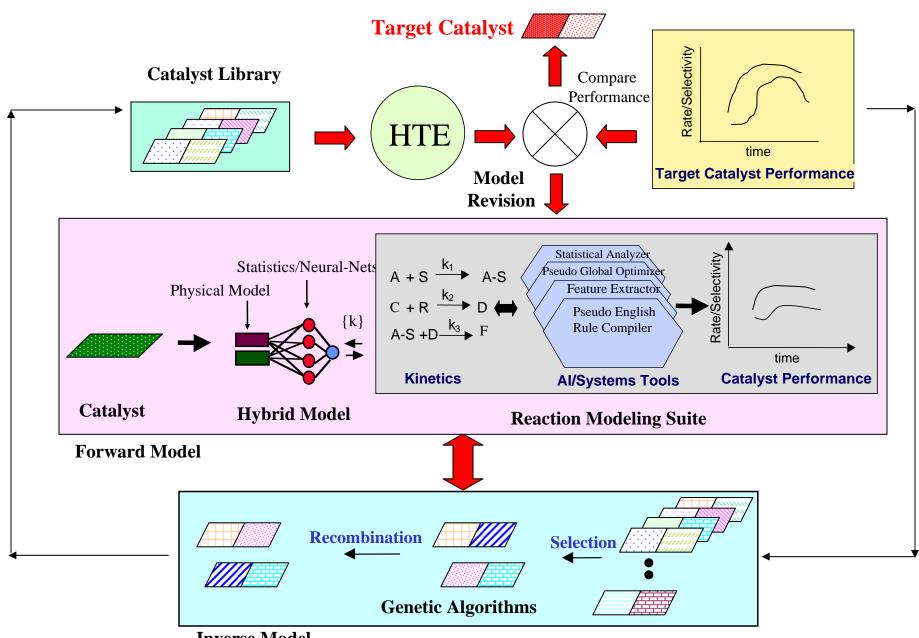
- Represents reaction chemistries explicitly
- Customizable for different catalyst chemistries
- Results
  - Real-time evaluation of 100s of reaction pathways and 1000s of DAEs
  - Saved months of model development effort
  - Improved mechanistic understanding and first principles models



**Proposed Framework for Knowledge Extraction from HTE – Kinetic Modeling** 



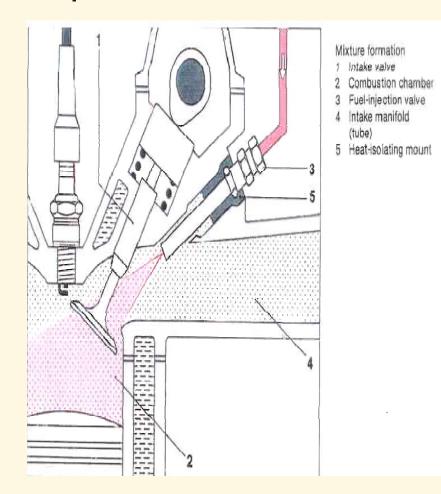
#### **Catalyst Design Challenge**



**Inverse Model** 

## LUBRIZOL: Fuel Additive Design

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- EPA requirement: Minimize intake-valve deposits (IVD)
- Approach: Fuel Additives

#### Performance measure

- BMW Test for IVD
- Stipulated to be less than 100 mg over a 10,000 mile road test

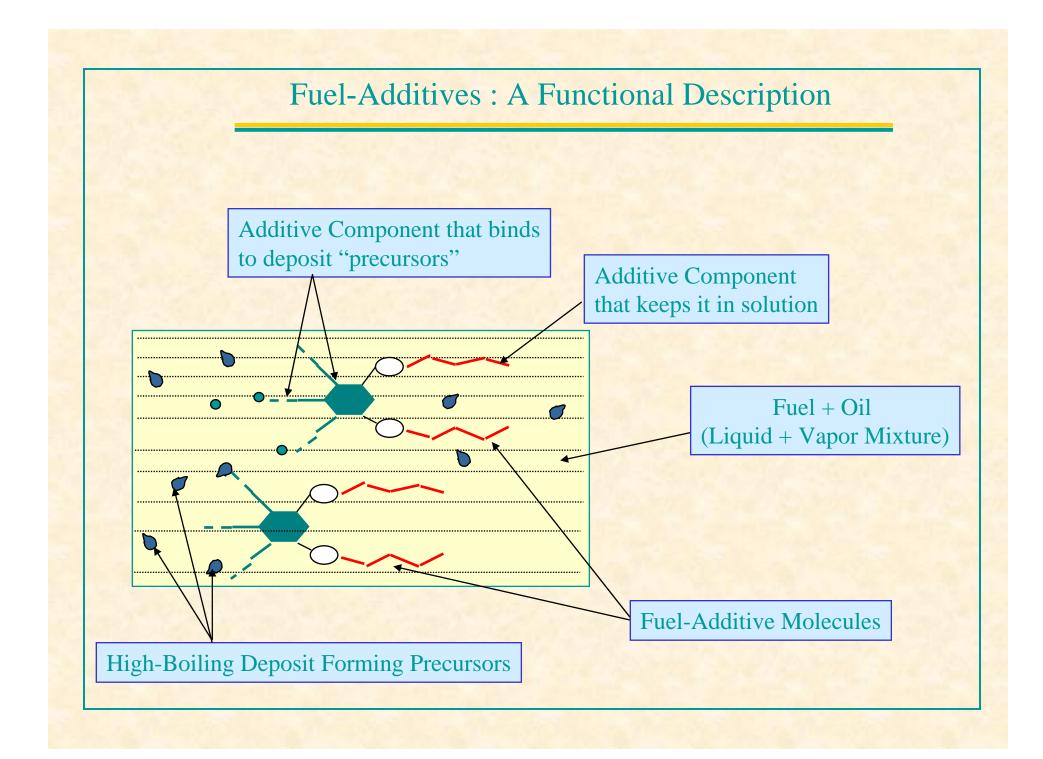
## Expensive and time-consuming testing

Around \$8000 for a single datum

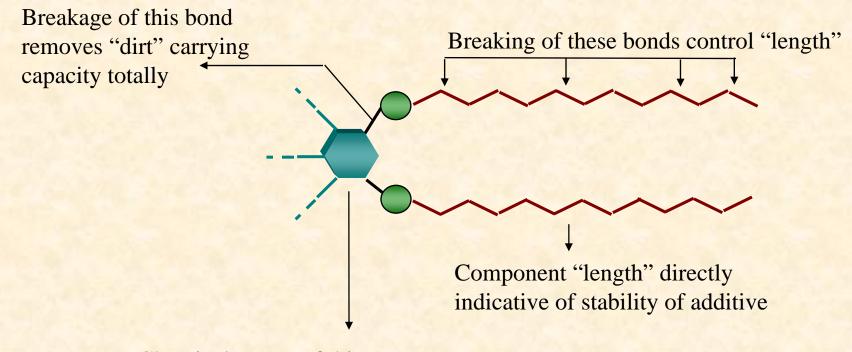
 Problem: Design fuel-additives that meet desired IVD performance levels

#### **Intake Valve and Manifold**





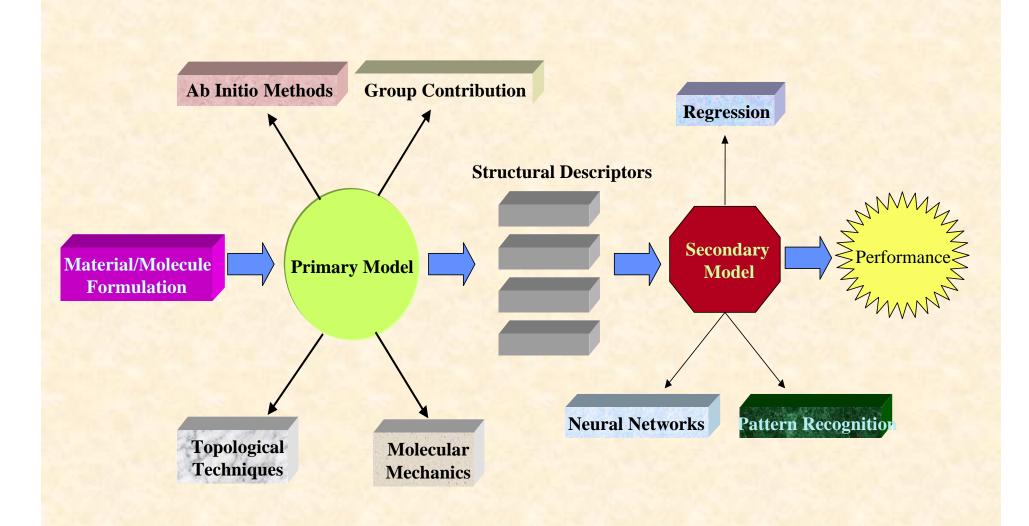
## First-Principles Model for Additive Degradation



Chemical nature of this component (polar/non-polar) controls "dirt" removing capacity

The first-principle model tracks the structural distribution of fuel-additive with time due to reactive degradation

## General Framework of Predictor Models



## Modeling Degradation

#### Dynamic in nature

- Modeled as first-order irreversible reactions for additive degradation
- Rate constants in proportion to rates of pure thermal degradation

Distribution of molecular species differing in structure
 Identified by effective "length"
 Population balance model tracks distribution with time

### From Stability to IVD

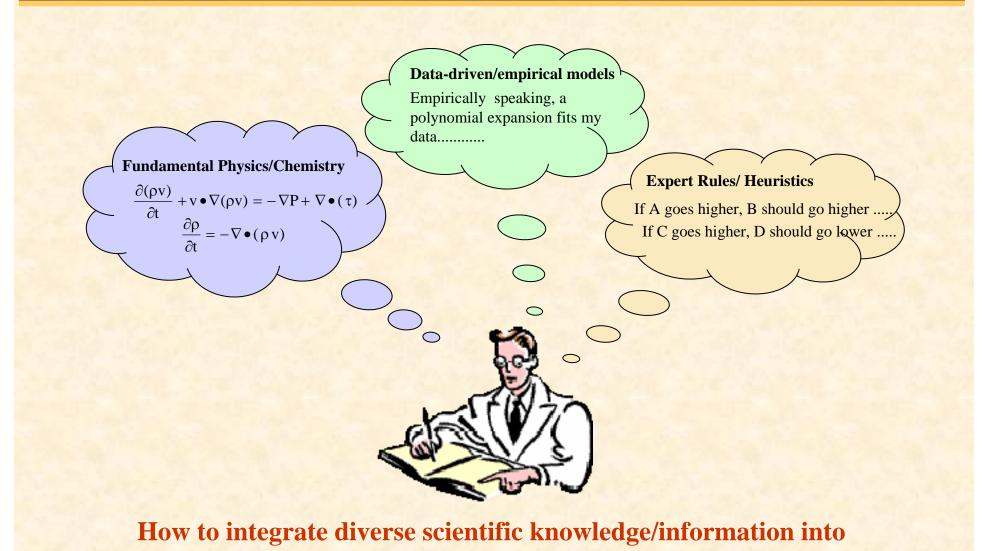
Define "amount of active additive"

The fraction of the additive species that remains active (i.e. intact viable structure) in the fuel at any point of time

A dynamic quantity decreasing with time

- Depends on additive distribution
- Solubility correlated to IVD via regression
  - Linear models
  - Neural-Network models
  - Input descriptors are the *amounts of active additive* at different times

#### Forward Problem Approaches



a single unified knowledge architecture ?



# All models are wrong.... ... but some are useful! -- George Box

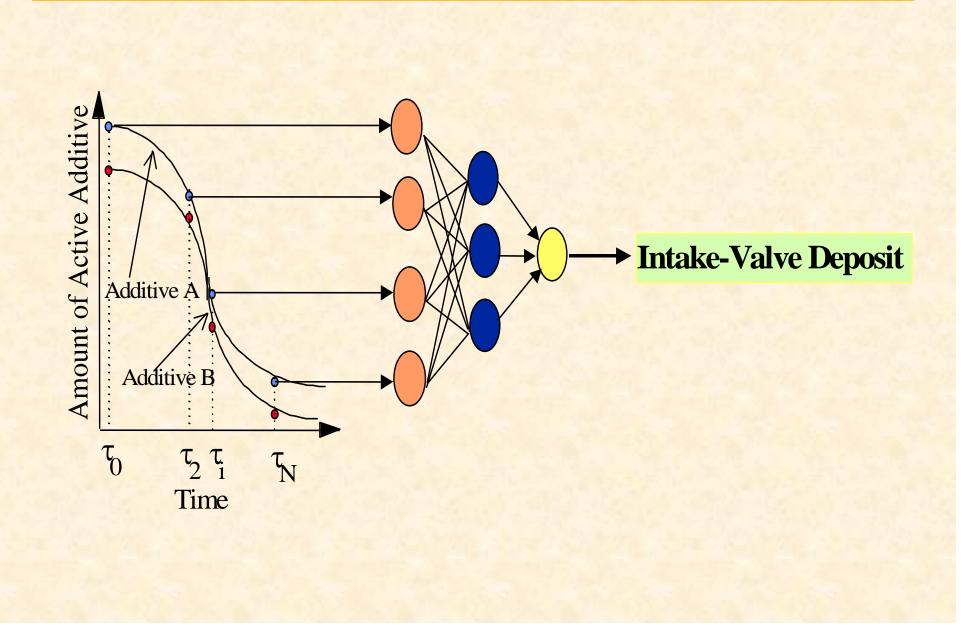
(U. Wisconsin)

## Hybrid Models Combine First-principles and Data-driven models

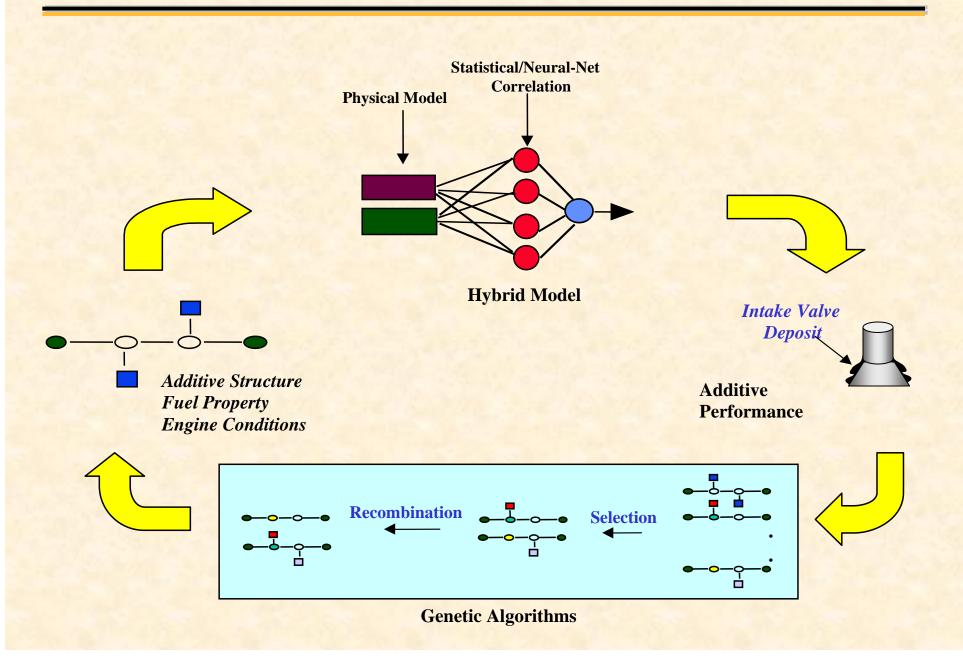


Venkat Venkatasubramanian, Plenary Lecture, Foundations of Computer-Aided Process Design, Princeton, July 2004.

## Hybrid Model for IVD Prediction



## Computer-Aided Design of Fuel-Additives



## Previous Approaches to Inverse Problem

#### Previous Methodologies

- Random Search
- Heuristic Enumeration
- Math Programming
- Knowledge-Based Systems
- Graph Reconstruction
- Disadvantages
  - Combinatorial Complexity
    - Sonlinear Search Spaces
    - **~** Local Minima Traps
  - Difficulties in Knowledge Acquisition
  - Difficulties in using high-level chemical/bio-chemical knowledge

## **Overview of Genetic Algorithms**

#### Definition

Genetic Algorithms are stochastic, evolutionary search procedures based on Darwinian model of natural selection Evolution = Random Change + Survival of the fittest

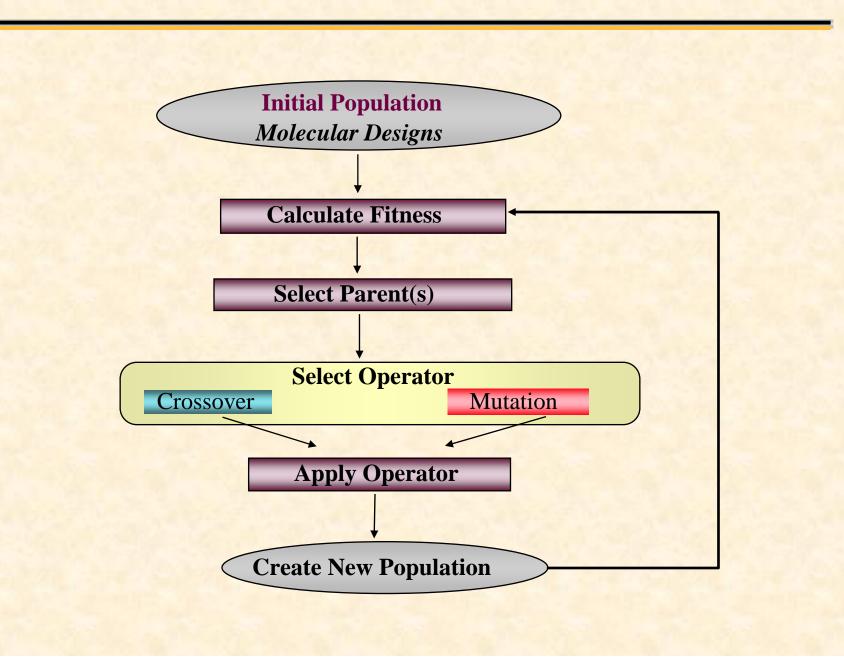
- Essential Components
  - Genetic Operators
    - Crossover
    - Mutation
  - Reproductive Plan
    - Fitness Proportionate Selection

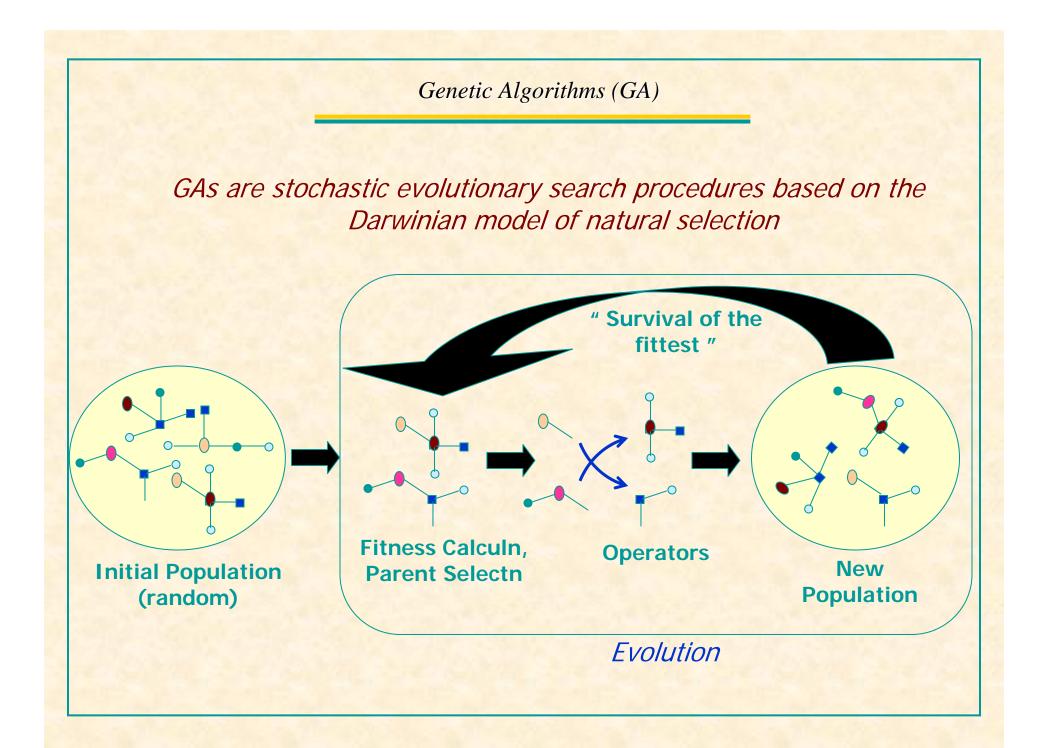
## Genetic Algorithms for Product Design

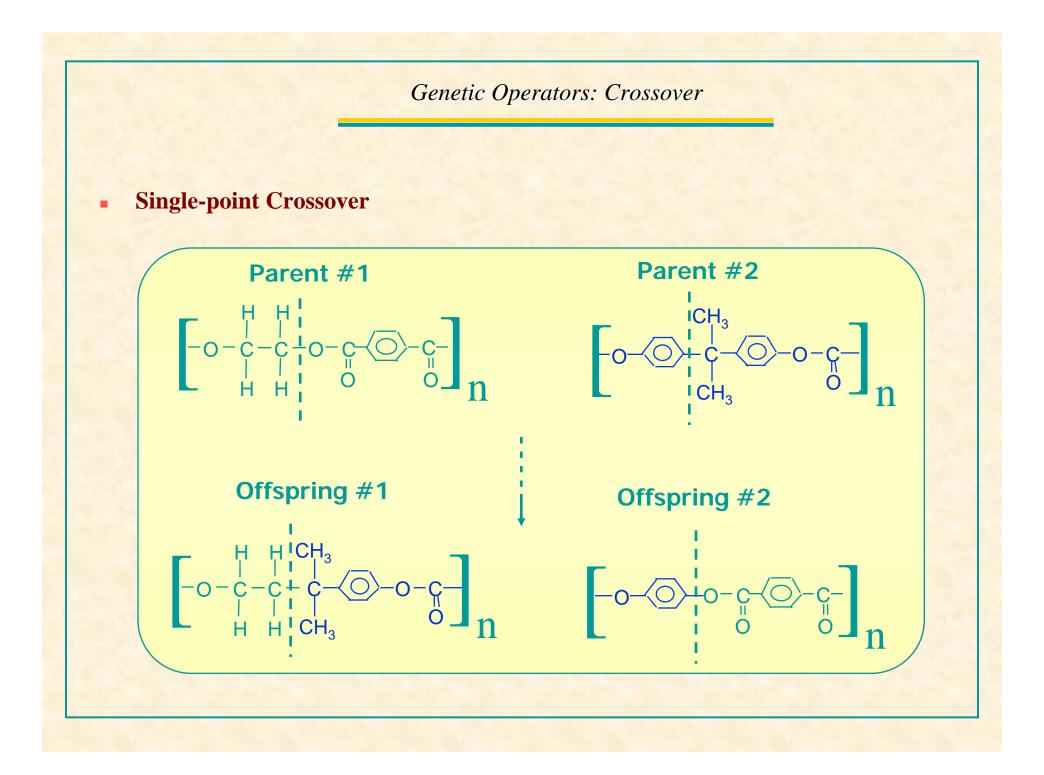
#### Global Search

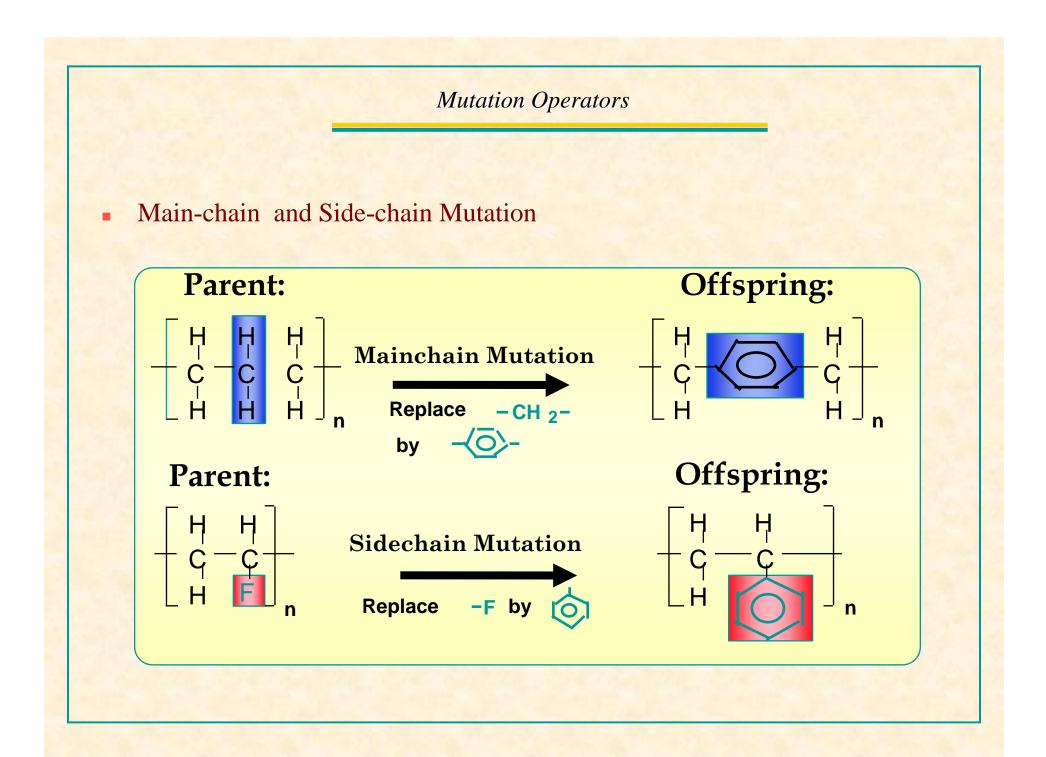
- Diversity of solutions
- High potential for novelty
- Global Optima
- Development is de-coupled from forward problem
  - Robust to non-linearity
- Population based search
  - Ability to provide several near-optimal solutions
- Captures transparently the rich chemistry of the design problem

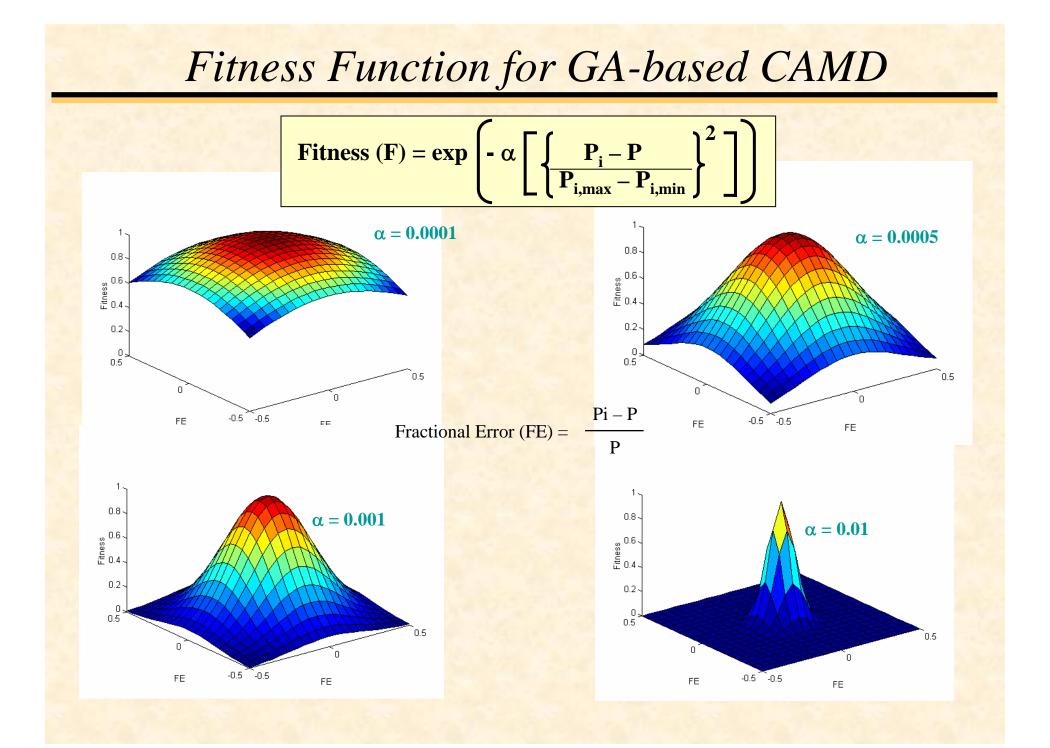
## **Overview of Genetic Algorithms**











## Polymer Design Case Study

#### • Base Groups

17 Main-chain Groups			<u>15 Side-chain Groups</u>				
>C<	2	-ONH-	-H	-CH <sub>3</sub>	-C <sub>2</sub> H <sub>5</sub>	-nC <sub>3</sub> H <sub>7</sub>	-iC <sub>3</sub> H <sub>7</sub>
0 '' -C-	O O -O-CO-C-	0 0          0C-O-C-	tC <sub>4</sub> H9	-F	-C1	-Br	-OH
О " -С-NH-	0 0 -O-C-NHNHC	-NH{O}-	-ОСӉ	О -О-С-СН3	О С-СНз	0	-CN
101	<u>v</u>	$x \rightarrow x$					

#### Target Properties

• Density

- Glass Transition Temperature
- Thermal Expansion Coefficient
- Specific Heat Capacity

• Bulk Modulus

## Target Properties

Target Polymer	Density (gm/cm <sup>3</sup> )	Glass Transition (K)	Thermal Expansion 1/K	Heat Capacity J/kg K	Bulk Modulus K N/m <sup>3</sup>
TP1: $- \underbrace{\circ}_{\circ} - $	1.34	350.75	2.96x10 <sup>-4</sup>	1152.67	5.18x10 <sup>9</sup>
TP2: $\left[ \begin{array}{c} - c \\ - c \\ - c \\ - r \\ - r$	1.18	225.24	2.81x10 <sup>-4</sup>	1377.82	2.51x10 <sup>9</sup>
TP3: $- \left\{ \circ - \circ $	1.21	420.83	2.90x10 <sup>-4</sup>	1135.10	5.40x10 <sup>9</sup>
$TP4:  - \underbrace{ \left< \bigcirc {}^{\circ} {}^{$	1.19	406.83	2.90x10 <sup>-4</sup>	1073.96	5.39x10 <sup>9</sup>
TP5: $-\left( \bigcirc -\infty \right)_{n}$	1.28	472.00	2.89x10 <sup>-4</sup>	995.95	5.31x10 <sup>9</sup>
$TP6: \qquad \left\{ \circ - \bigcirc - \circ - \bigcirc - \circ - \circ \right\}_{n}$	1.25	421.12	2.90x10 <sup>-4</sup>	1016.55	6.12x10 <sup>9</sup>
TP7: $-\begin{bmatrix} \begin{matrix} \mu \\ \nu \\ \mu \end{matrix} - \begin{matrix} \mu \\ \nu \end{matrix} - \begin{matrix} \mu \\ \nu \end{matrix} - \begin{matrix} \mu \\ \mu \end{matrix} - \begin{matrix} \mu \end{matrix} - \begin{matrix} \mu \\ \mu \end{matrix} - \begin{matrix} \mu \end{matrix} - \begin{matrix} \mu \end{matrix} - \begin{matrix} \mu \\ \mu \end{matrix} - \begin{matrix} \mu \end{matrix} - \begin{matrix} \mu \\ \mu \end{matrix} - \begin{matrix} \mu \end{matrix} - \end{matrix} - \begin{matrix} \mu \end{matrix} - \begin{matrix} \mu \end{matrix} - \end{matrix} - \begin{matrix} \mu \end{matrix} - \end{matrix} - \end{matrix} - \begin{matrix} \mu \end{matrix} - $	1.06	322.55	2.98x10 <sup>-4</sup>	1455.90	3.85x10 <sup>9</sup>

## Polymer Design Case Study: Results

Target Polymer	Random MC, SC	Random MC, SC Feasibility Constraints
$ \begin{array}{c} \begin{array}{c} \begin{array}{c} & & & \\ & & \\ \end{array} \\ \hline \\ & \\ & \\ & \\ \end{array} \\ 0 \end{array} \\ \begin{array}{c} \\ \\ \\ \\ \\ \end{array} \\ \hline \\ \\ \\ \\ \\ \\ \end{array} \\ \begin{array}{c} \\ \\ \\ \\ \\ \\ \\ \end{array} \\ \\ \\ \\ \\ \\ \end{array} \\ \begin{array}{c} \\ \\ \\ \\ \\ \\ \\ \\ \end{array} \\ \\ \\ \\ \\ \\ \\ \end{array} \\ \begin{array}{c} \\ \\ \\ \\ \\ \\ \\ \\ \end{array} \\ \\ \\ \\ \\ \\ \\ \\ \end{array} \\ \begin{array}{c} \\ \\ \\ \\ \\ \\ \\ \\ \\ \end{array} \\ \\ \\ \\ \\ \\ \\ \\ \\ $	12% 184 282	60% 240 213
$ \begin{array}{c c} H & F & H & H \\ \hline C & -C & -C & -C \\ \hline L & I & I & I \\ -H & F & H & CH_{3} \end{bmatrix} n $	36% 411 6	48% 522 6
$- \underbrace{\begin{bmatrix} 0 - \mathbf{C} - 0 \\ \mathbf{H} \\ 0 \end{bmatrix}}_{0} \underbrace{\begin{bmatrix} \mathbf{C} \mathbf{H} \\ 0 \\ \mathbf{C} \mathbf{H} \\ 0 \end{bmatrix}}_{\mathbf{n}} \underbrace{\begin{bmatrix} \mathbf{C} \mathbf{H} \\ 0 \end{bmatrix}}_{\mathbf{n}}$	0% 	12% 193 74
	0% - 861	0% 
	32% 400 175	48% 232 142
	8% 548 199	32% 632 168
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	100% 61 217	100% 64 198
$ \begin{array}{c} \hline 0 & - \begin{array}{c} c \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\$	68% 210 162	88% 109 161
	8% 382 144	4% 868 70

Legend: Success Rate; Average Conv. Generation; Number with fitness >0.99

## Near Optimal Designs

Polymer Design	<b>Overall Error</b>	Fitness
C H 3         C H 3       C H 3         C H 3       C H 3         C H 3       C H 3         C H 3       C H 3	0%	1.0
Case 1: Standard GA		
$\begin{bmatrix} & & & \\ $	0.74%	0.995
$\begin{bmatrix} C_{2}H_{5} \\ -C_{2}H_{5} \\$	1.18%	0.991
Case 2: Modified GA, Stability $\begin{bmatrix} 0 & H & 0 \\ 0 & H & 0 \\ 0 & -C & -C & -C & -0 & -C & -0 \end{bmatrix}_{n}$ $\begin{bmatrix} 0 & C_{2}H_{5} \\ -C & -0 & -C & -S & -0 & -0 \end{bmatrix}$	0.25%	0.999
$ \underbrace{\begin{bmatrix} 0 & C_2H_5 \\ C' - 0 & -C' - S & -C' & -C' & -C' \\ H & H & -C' & -C' & -C' & -C' & -C' \\ H & H & -C' &$	1.10%	0.991
Case 3: Modified GA, Stability & Complexity		
	0.21%	0.999
$\begin{bmatrix} H & 0 & 0 \\ C & -0 & -C \\ H & 3 \\ \hline C & H & 3 \\ \hline 0 & -0 & -C & -C \\ \hline 0 & -0 & -C & -0 \\ \hline 0 & -0 & -C \\ \hline 0 & -0$	0.83%	0.995

## Advantages of GAs for Product Design

#### Global Search

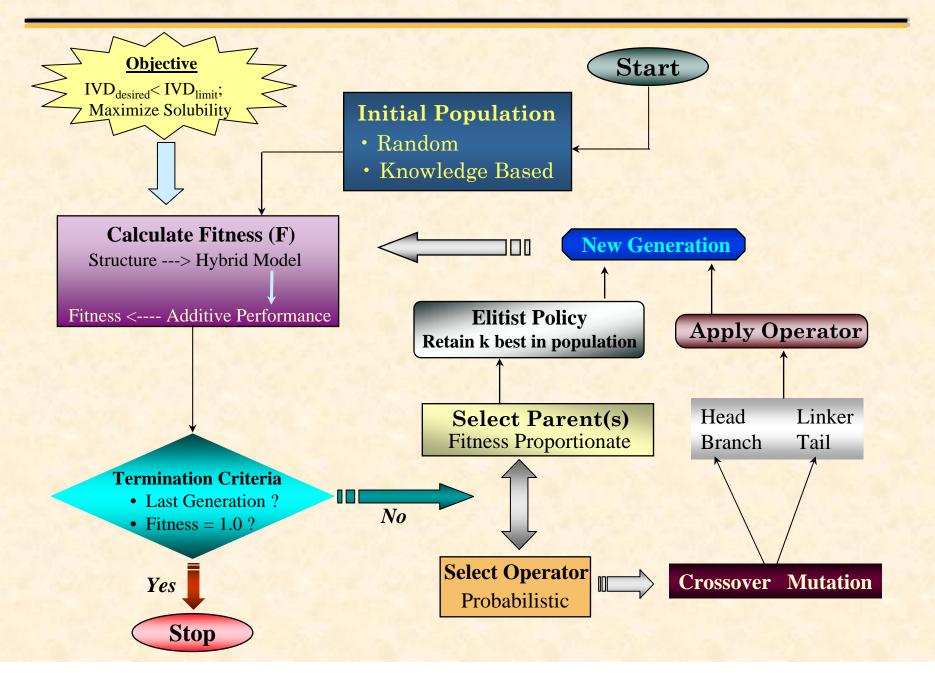
- Diversity of solutions
- High potential for novelty
- Global Optima
- Development is de-coupled from forward problem
  - Robust to non-linearity
- Population based search
  - Ability to provide several near-optimal solutions
- Captures transparently the rich chemistry of the design problem

## Drawbacks of GAs

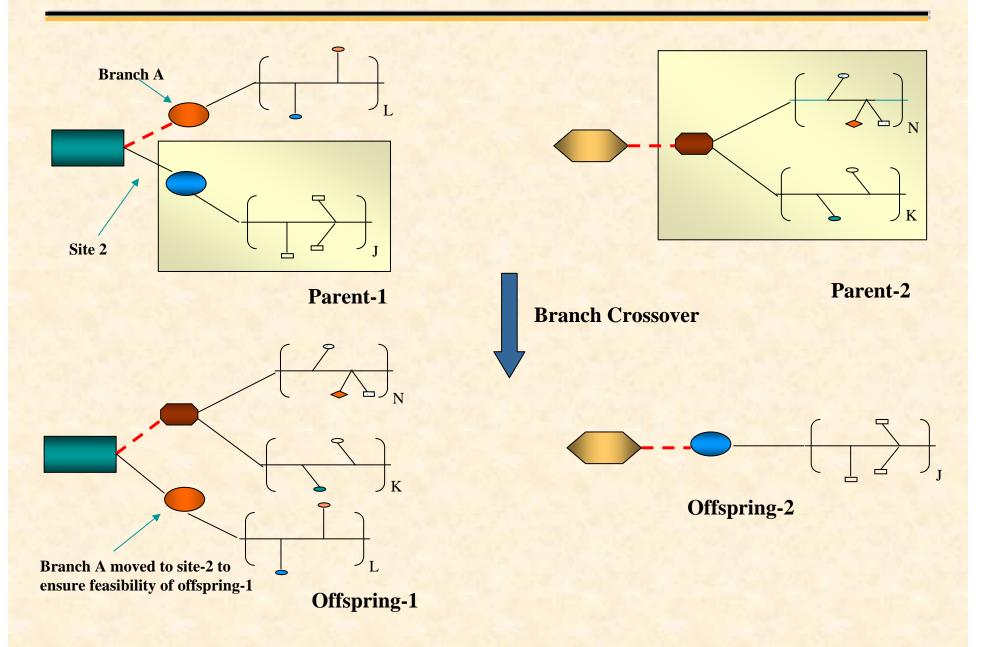
Powerful generic method with some drawbacks

- No convergence guarantees
- Performance sensitive to parameters
- Performance dependent on search space structure

## Evolutionary Design of Fuel-Additives



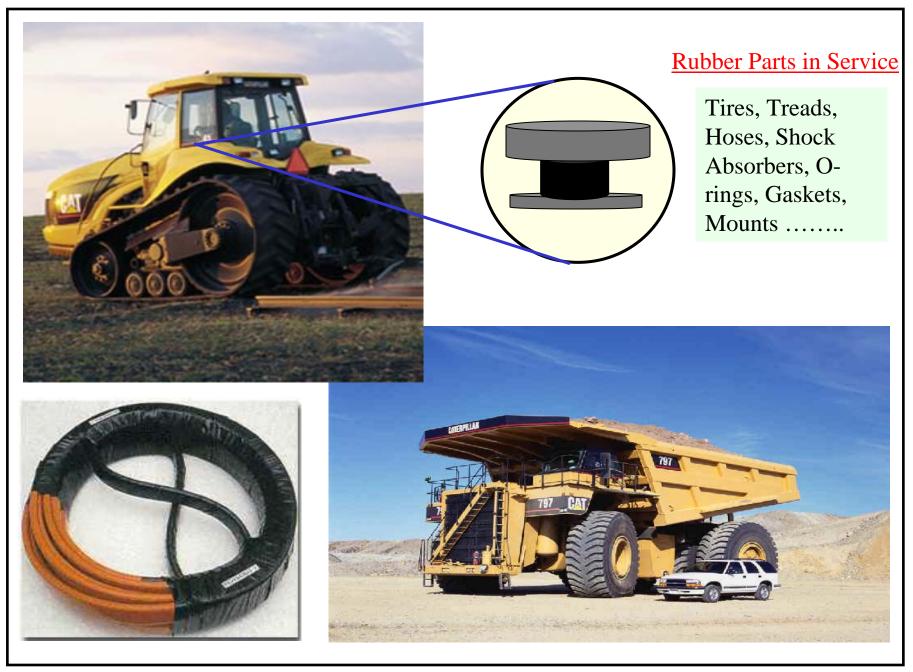
## Genetic Operators: Branch Crossover



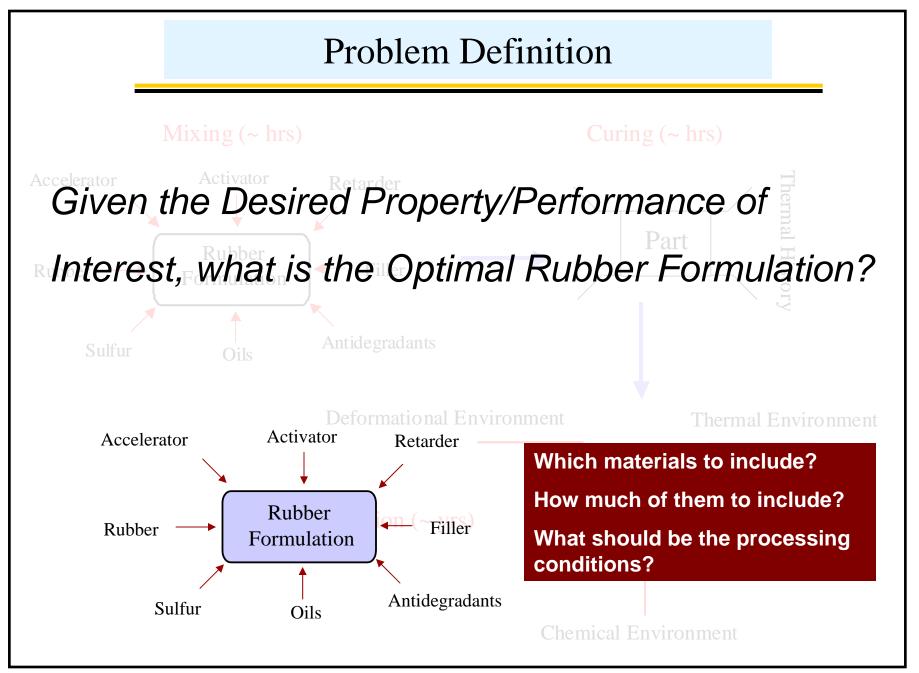
## Evolutionary Design of Fuel Additives: Results

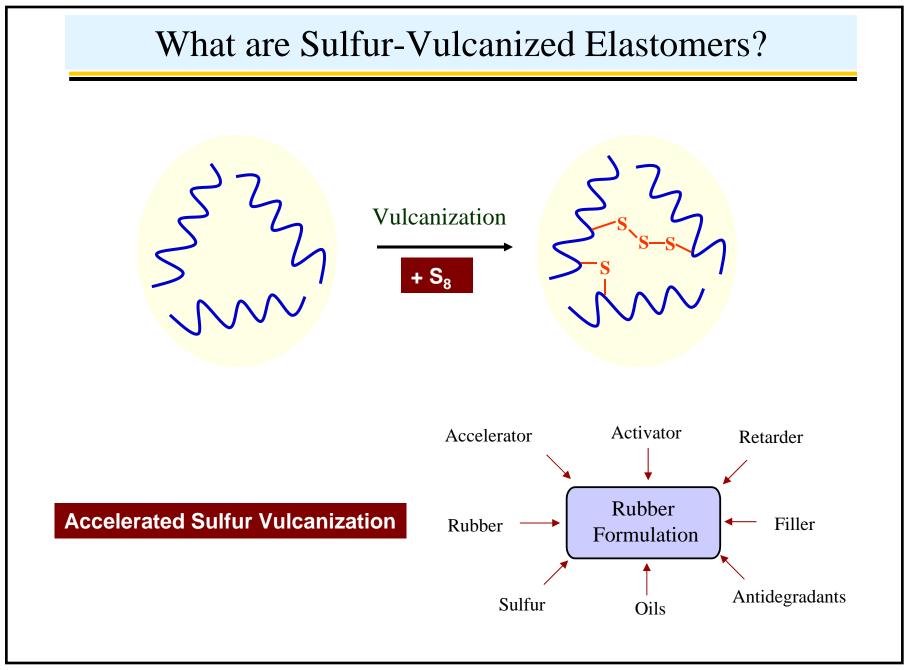
#### **Objective: Determine a structure with IVD < 10 mg Dosage: 50 PTB; Population Size: 25; Generations: 25**

Run	Rank/Identifier	Fitness	Predicted IVD (PLS-NN Model)	Structural Description		
	1, I-1	0.997	11.4 mg	Novel Structure. Infrequently used linker.		
I	2, I-2	0.996	11.5 mg	Novel Structure. Same tails as best structure, different heads and linkers		
	6, I-6	0.993	12.0 mg	Variant of structure found in the BMW database. Same head and linkers, different tails		
	1, II-1	0.999	10.1 mg	Novel Structure. Different from <i>I-1</i> . Infrequently used linker component.		
п	2, II-2	0.989	12.6 mg	Slight variant of additive structure found in BMW and HONDA databases. Different tails but same head and linker		
	4, II-4	0.983	13.2 mg	Minor variation of structure <i>II-2</i> above. Slight modification of the head		
	1, III-1	1.00	8.9 mg	Novel Structure. Different from <i>I-1</i> and <i>II-1</i> . Commonly used components		
ш	2, III-2	0.994	<b>11.9</b> mg	Variant of <i>III-1</i> . One linker and tail modified.		
	3, III-3	0.993	12.1 mg	Variant of structure <i>II-2</i> above. Slight modification of head. A linker and tail inserted.		

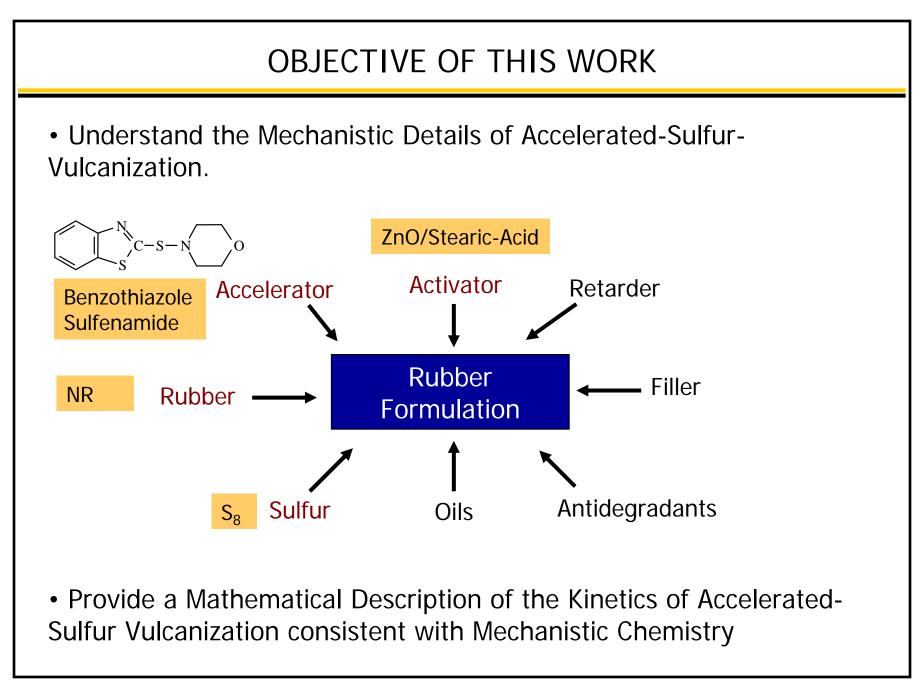


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#### COMPLEXITY OF VULCANIZATION REACTIONS

W.Scheele (1956) <sup>1</sup> Perhaps no-where in chemistry is there encountered a field which even in its literature alone shows so many uncertainties and (possibly only apparent) contradictions as that of the vulcanization of rubber.

<sup>1</sup>W. Scheele, O. Lorenz and W. Dummer, Rubber Chemistry and Technology, 29, 1 (1956)

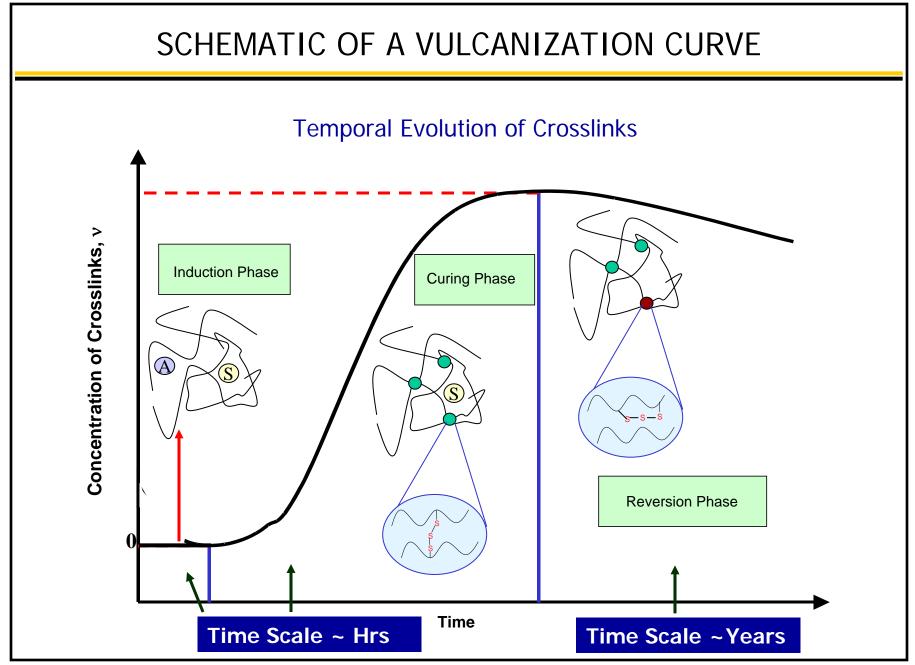
L.Bateman (1963) <sup>2</sup> Whilst it has long been appreciated, albeit intuitively, that sulfur vulcanization is a very complex chemical process, the actual complexity as revealed in the studies described above is probably far in excess of what has ever been envisaged.

<sup>2</sup> L. Bateman, C.G. Moore, M. Porter and B. Saville, *"The Chemistry and Physics of Rubber-Like Substances"*, L Bateman, Ed., Maclaren & Sons Ltd., London, 1963, pp 449.

P.J. Nieuwenhuizen (1997) <sup>3</sup> It must be considered remarkable that despite all the efforts and progress in the field of vulcanization during the past decade, one has to conclude that the statements of Scheele and Bateman, made 30 to 40 years ago, are still true to a great extent.

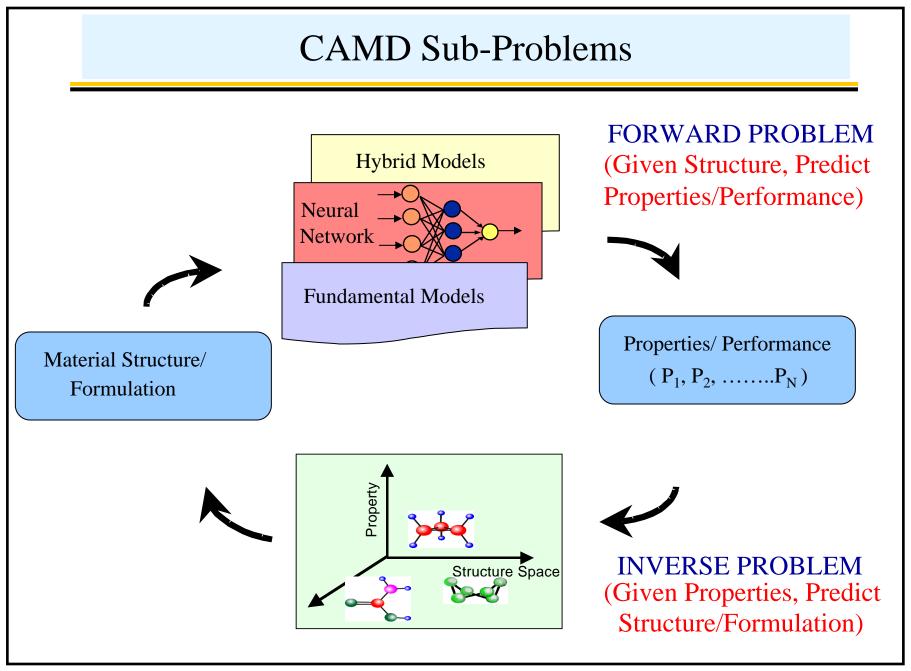
<sup>3</sup> P.J. Nieuwenhuizen, Rubber Reviews, Rubber Chemistry and Technology, 29, 70 (1997)

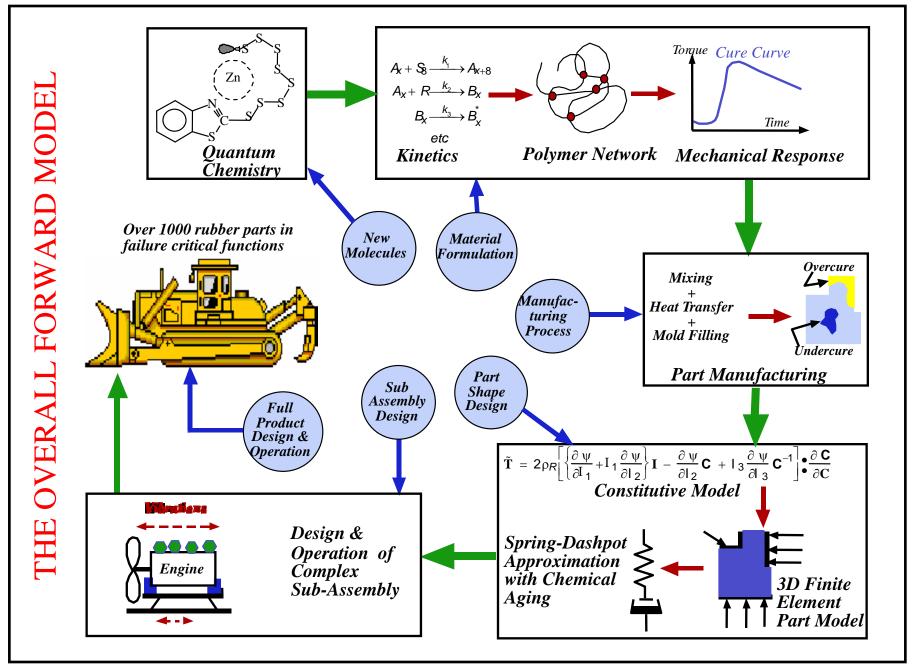
AIChE Annual Meeting, Reno 2001



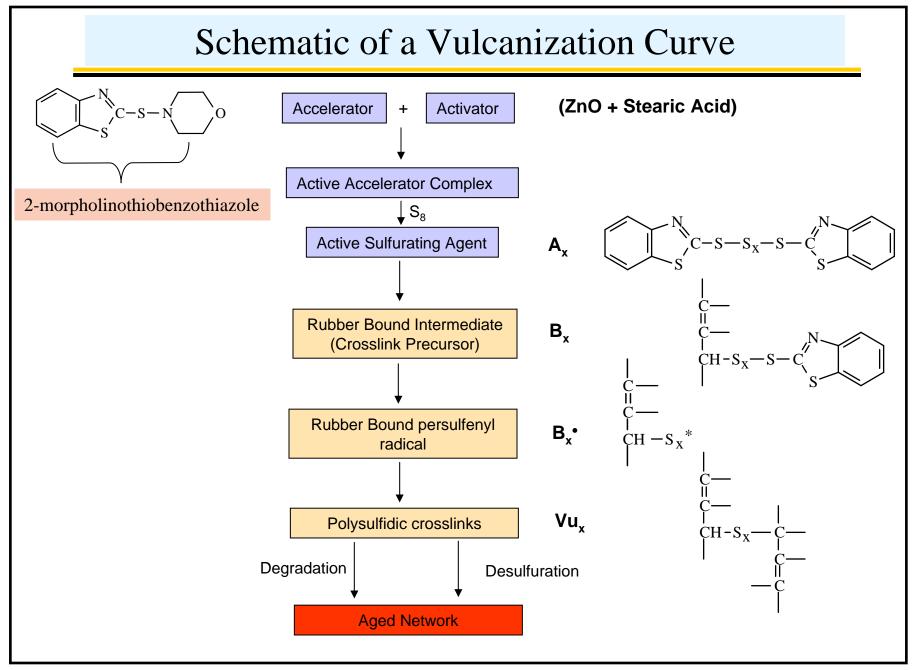
AIChE Annual Meeting, Reno 2001

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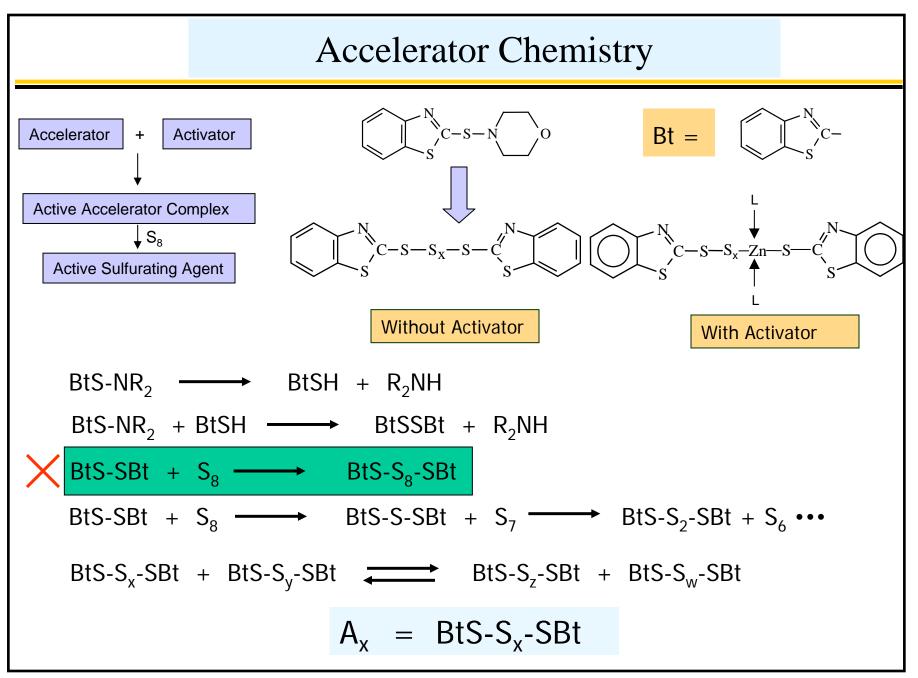




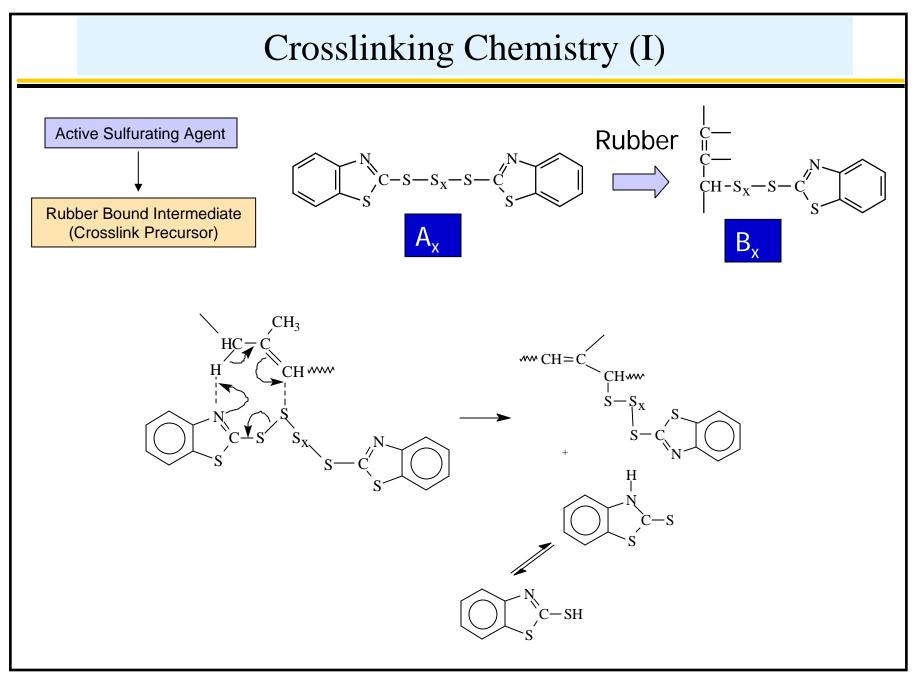
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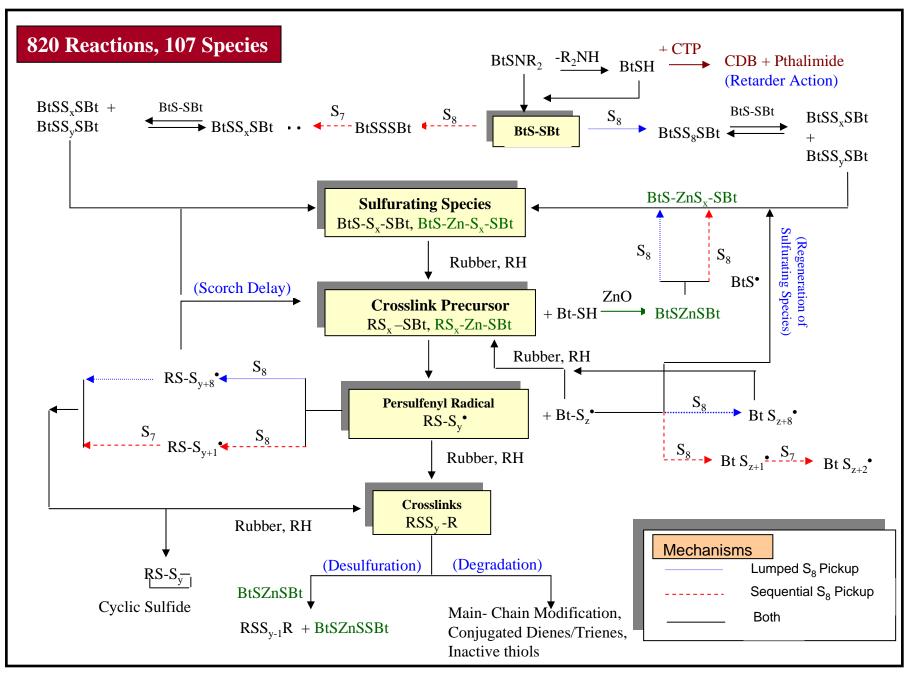
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#### POPULATION BALANCE EQUATIONS

Equations for MBTS and other sulfurating species

$$\begin{split} \frac{d}{dt} \Big[ A_0 \Big] &= k_{MBS} [MBS] - k_{MBS-MBT} [MBT] [MBS] - k_{A-A} [A_0] \sum_{r=2}^{14} (r-1) A_r - k_{A-S} [A_0] [S_8] \\ &- k_{A-R} [A_0] - k_{A-BST} [A_0] \sum_{r=1}^{16} B^* r + 0.5 k_{E-E} [E_0^*]^2 - k_{DESULF} [A_0] \sum_{r=2}^{16} Vu_r + \\ &\begin{bmatrix} [A_1]^2 + 2[A_1][A_2] + 2 \left\{ [A_1][A_3] + 0.5[A_2]^2 \right\} + 2 \left\{ [A_1][A_4] + [A_2][A_3] \right\} + \\ 2 \left\{ [A_1][A_5] + [A_2][A_4] + 0.5[A_3]^2 \right\} + 2 \left\{ [A_1][A_6] + [A_2][A_5] + [A_3][A_4] \right\} + \\ 2 \left\{ [A_1][A_5] + [A_2][A_6] + [A_3][A_5] + 0.5[A_4]^2 \right\} + \\ 2 \left\{ [A_1][A_8] + [A_2][A_7] + [A_3][A_6] + [A_4][A_6] + 0.5[A_5]^2 \right\} + \\ 2 \left\{ [A_1][A_9] + [A_2][A_8] + [A_3][A_7] + [A_4][A_6] + 0.5[A_5]^2 \right\} + \\ 2 \left\{ [A_1][A_{10}] + [A_2][A_9] + [A_3][A_8] + [A_4][A_7] + [A_5][A_6] \right\} + \\ 2 \left\{ [A_1][A_{11}] + [A_2][A_{10}] + [A_3][A_{10}] + [A_4][A_8] + [A_5][A_7] + 0.5[A_6]^2 \right\} + \\ 2 \left\{ [A_1][A_{12}] + [A_2][A_{11}] + [A_3][A_{11}] + [A_4][A_{10}] + [A_5][A_9] + [A_6][A_8] + 0.5[A_7]^2 \right\} + \\ \frac{d}{dt} \Big[ A_1 \Big] = -2k_{A-R} \Big[ A_1 \Big] - k_{A-S} \Big[ A_1 \Big] \Big[ S_8 \Big] + 2k_{A-A} \Big[ A_0 \Big] \sum_{r=2}^{14} A_r + k_{DESULF} \Big[ A_0 \Big] \sum_{r=2}^{16} Vu_r \Big] \end{split}$$

$$-2k_{A-A}[A_1]\sum_{r=1}^{13}A_r + k_{E-E}[E_0^*][E_1^*]$$

#### POPULATION BALANCE EQUATIONS

Equations for MBTS and other sulfurating species

$$\frac{d}{dt}[A_{0}] = k_{A2}[MBT][MBS] - k_{A3}[A_{0}][S_{8}] - k_{A4}[A_{0}]\left[\sum_{i=2}^{14}(i-1)A_{i}\right] - k_{C1}[A_{0}]\right]$$
$$-k_{C4}[A_{0}]\left[\sum_{i=1}^{16}B_{i}*\right] - k_{R1}[A_{0}]\left[\sum_{i=1}^{16}Vu_{i}\right]\right]$$
$$\frac{d}{dt}[A_{1}] = -2k_{C1}[A_{1}] - k_{A3}[A_{1}][S_{8}] - 2k_{A4}[MBTS][A_{1}] + k_{R1}[A_{0}]\left[\sum_{i=1}^{16}Vu_{i}\right]$$
$$\frac{d}{dt}[A_{i}] = -2k_{C1}[A_{i}] - k_{A3}[A_{i}]\left\{\begin{bmatrix}S_{8}], 2 \le i \le 6\\0, i > 7\end{bmatrix} - (i+1)k_{A4}[A_{0}][A_{i}] + k_{A3}[A_{i}]\left\{\begin{bmatrix}0, 2 \le i \le 6\\[S_{8}], i > 7\end{bmatrix}\right\}$$

Equations for Crosslink Precursors

$$\frac{d}{dt} [B_0] = (k_{C1} [MBTS] + k_{C7} [E_1^*])$$
  
$$\frac{d}{dt} [B_i] = -k_{A4} [A_0] [B_i^*] + 2k_{C1} [A_i] - (i-1)k_{C2} [B_i] + k_{C7} [E_{i+1}^*]$$

#### **RATE-CONSTANT DETERMINATION**

#### FACTS

Total of 820 different reactions107 Coupled Ordinary Nonlinear Differential Equations9 Optimizable Rate Constants

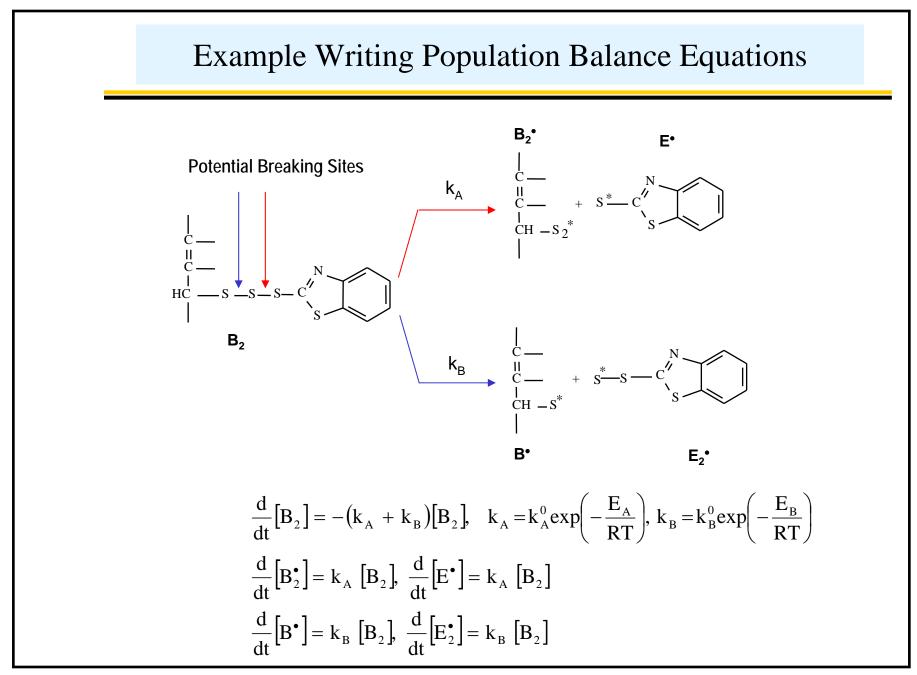
$$\min_{\mathbf{k}} \sum_{i=1}^{q} \sum_{j=1}^{m} \left[ \frac{v_{i,j}(\mathbf{k}) - v_{i,j}^{\exp}}{v_{i,j}^{\exp}} \right]^{2}, \quad \mathbf{k} = [k_{1}, k_{2}, k_{3}, \dots, k_{P}]$$
s.t. m time points, q concentrations  

$$\frac{d}{dt} [v] = \phi(v, c, \mathbf{k})$$

$$\mathbf{k} \ge 0$$

$$\mathbf{k} = Rate Constants$$

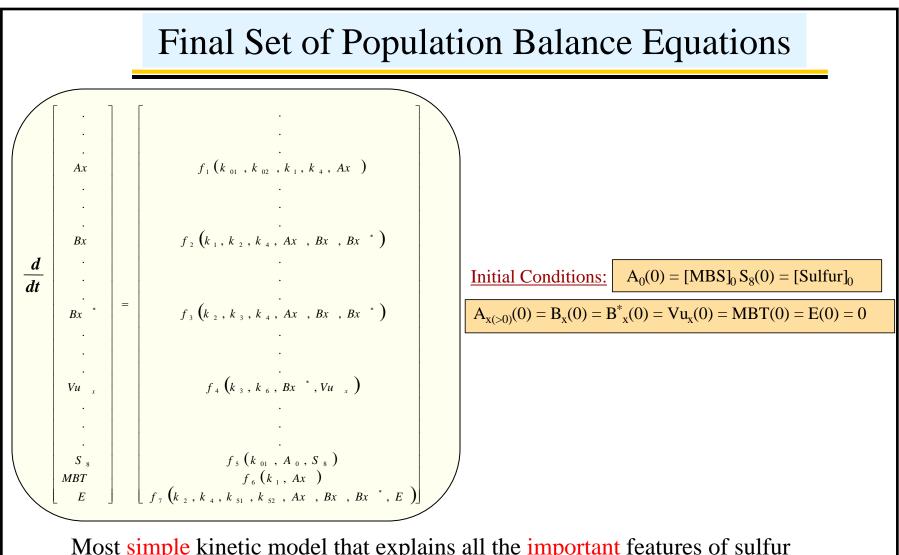
$$v_{i,j}^{\exp} = Experimental Data Point at time i and conc j$$



### **Population Balance Equations**

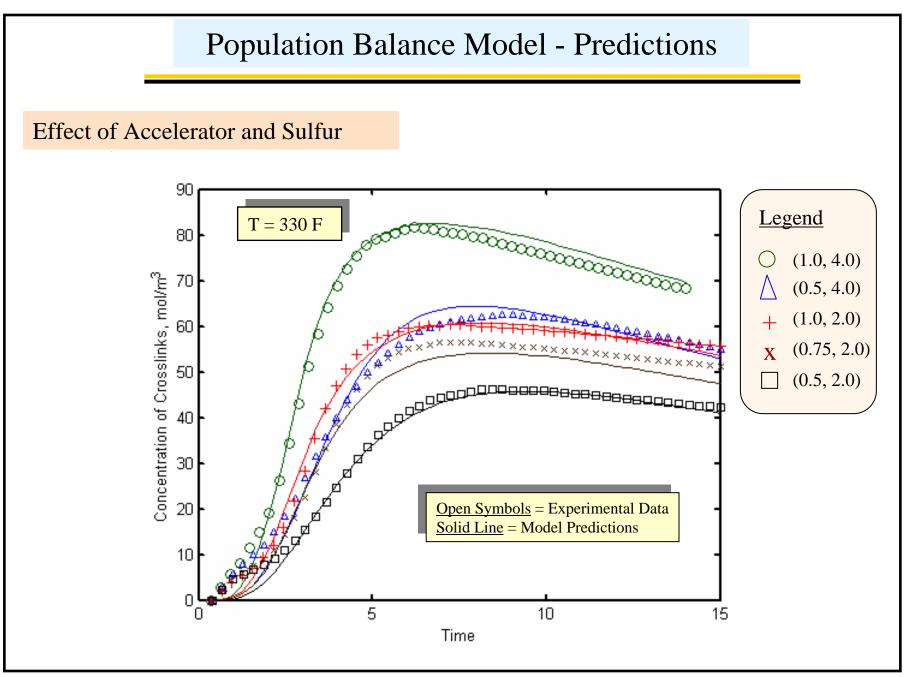
Equations for MBTS and other sulfurating species

$$\begin{split} \mathbf{x} &= \mathbf{0} & \frac{d}{dt} \Big[ A_0 \Big] = \mathbf{k}_{\text{MBS-MBT}} [\text{MBT}] [\text{MBS}] - \mathbf{k}_{\text{A-A}} [A_0] \sum_{r=2}^{14} (r-1) A_r - \mathbf{k}_{\text{A-S}} [A_0] \sum_{y=1}^{8} [S_y] \\ & -\mathbf{k}_{\text{A-R}} [A_0] - \mathbf{k}_{\text{A-BST}} [A_0] \sum_{r=1}^{16} B^* r + \frac{1}{2} \mathbf{k}_{\text{E-E}} [E_0^*]^2 - \mathbf{k}_{\text{DESULF}} [A_0] \sum_{r=2}^{16} \nabla \mathbf{u}_r \\ & + \mathbf{k}_{\text{A-A}} \sum_{x=1}^{13} \sum_{y=1}^{13-x} A_x A_y \\ \mathbf{x} &= \mathbf{1} & \frac{d}{dt} [A_1] = -2\mathbf{k}_{\text{A-R}} [A_1] - \mathbf{k}_{\text{A-S}} ([A_1] - [A_0]) \sum_{y=1}^{8} [S_y] + 2\mathbf{k}_{\text{A-A}} [A_0] \sum_{r=2}^{14} A_r + \mathbf{k}_{\text{DESULF}} [A_0] \sum_{r=2}^{16} \nabla \mathbf{u}_r \\ & -2\mathbf{k}_{\text{A-A}} [A_1] \sum_{r=1}^{13} A_r + \mathbf{k}_{\text{E-E}} [E_0^*] [E_1^*] \\ \mathbf{2} \leq \mathbf{x} \leq \mathbf{13} & \frac{d}{dt} [A_x] = -2\mathbf{k}_{\text{A-R}} [A_x] - \mathbf{k}_{\text{A-S}} ([A_x] - [A_{x-1}]) \sum_{y=1}^{8} [S_y] + 2\mathbf{k}_{\text{A-A}} [A_0] \sum_{r=x+1}^{14} A_r \\ & -(\mathbf{x}-1)\mathbf{k}_{\text{A-A}} [A_0] [A_x] - 2\mathbf{k}_{\text{A-A}} [A_x] \sum_{r=1}^{14x} A_r + \mathbf{k}_{\text{E-E}} [E_0^*] [E_x^*] \\ & + \mathbf{k}_{\text{A-A}} \sum_{r=1}^{x-1} [A_r] [A_{x,r}] \end{split}$$

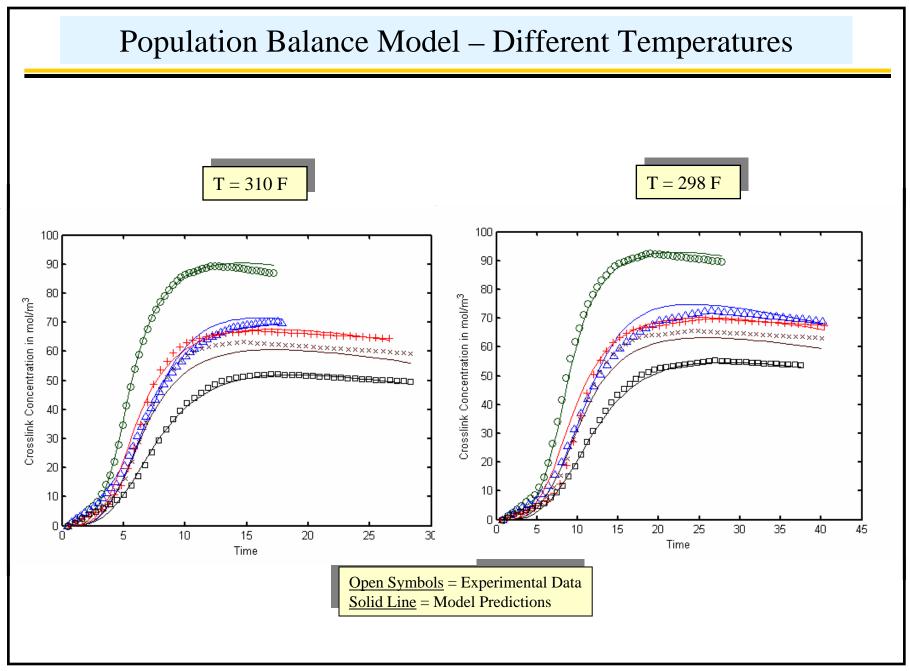


Most simple kinetic model that explains all the important features of sulfur vulcanization.

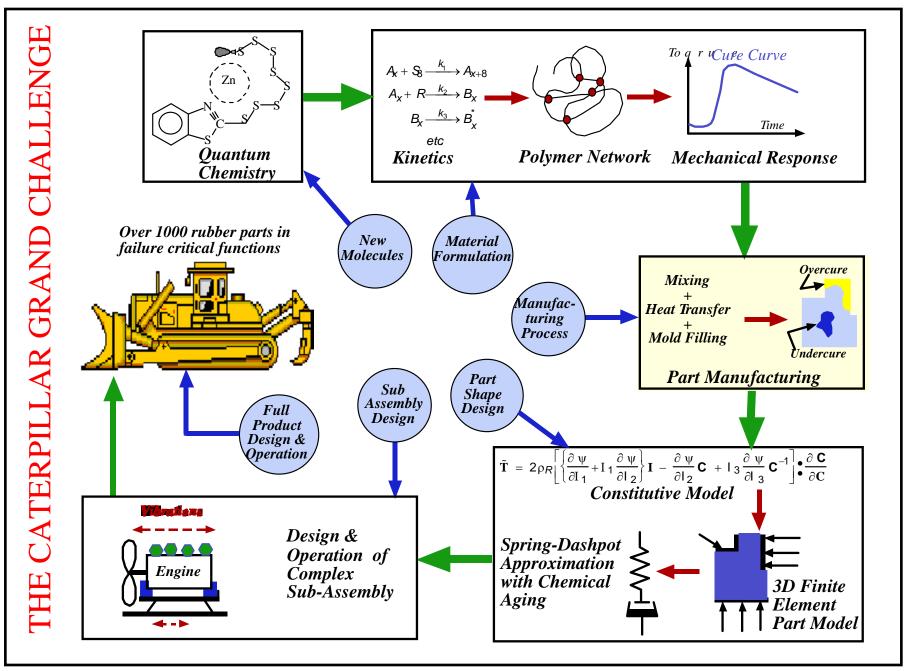
Total of 820 different reactions considered with 107 coupled ordinary nonlinear differential equations and 9 optimizable rate-constants.



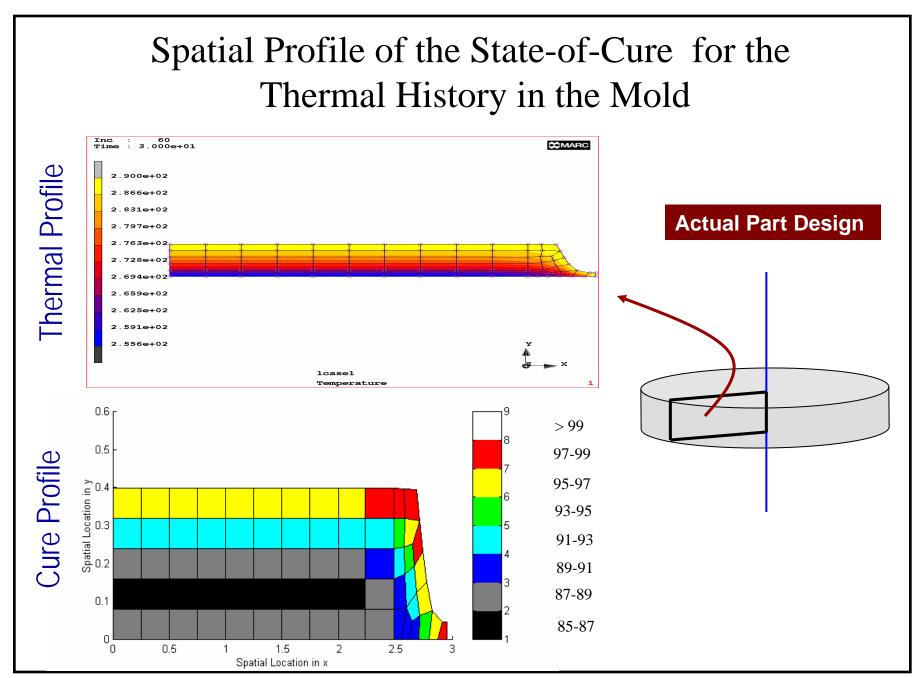
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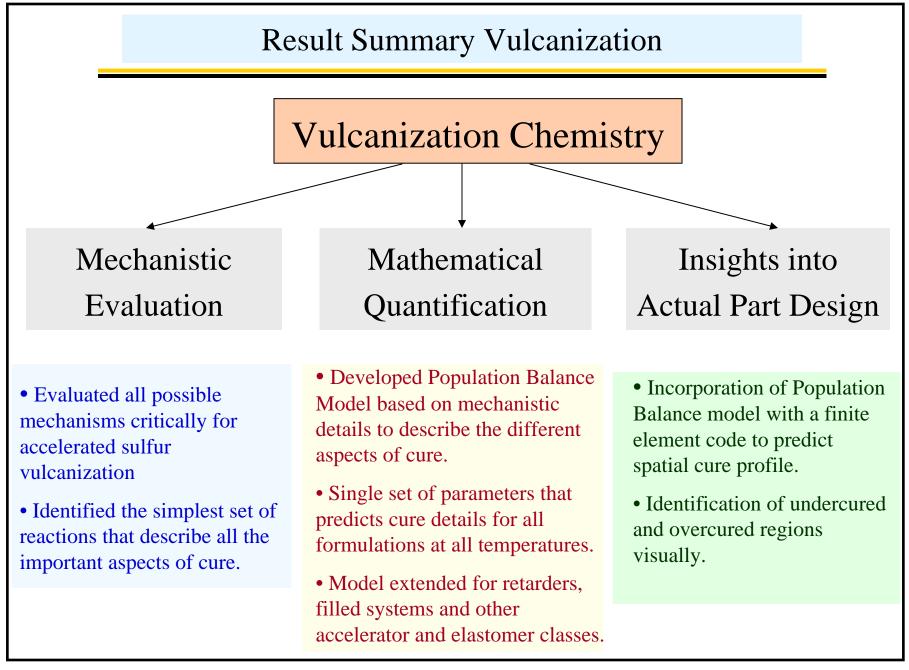
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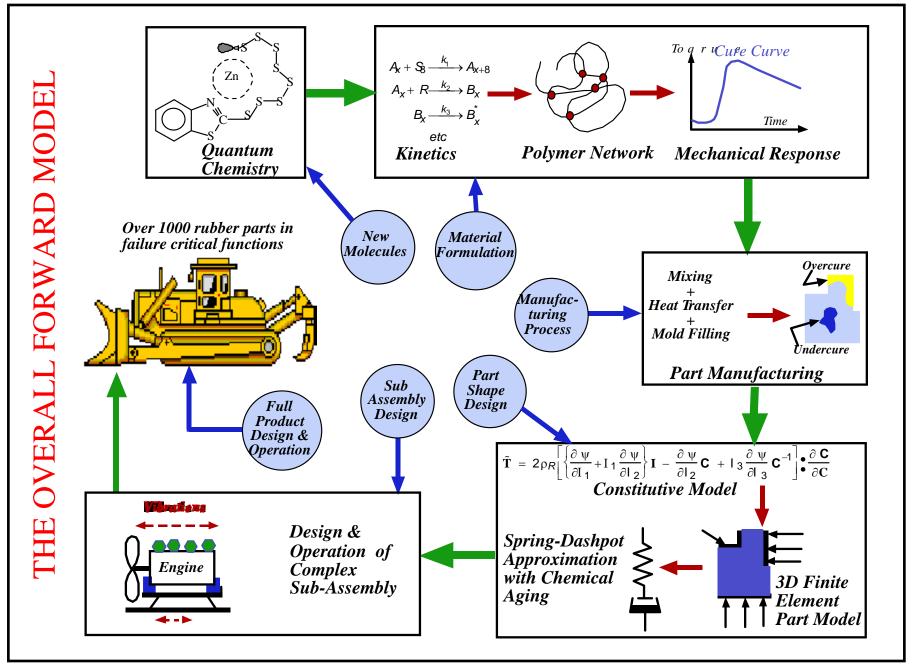


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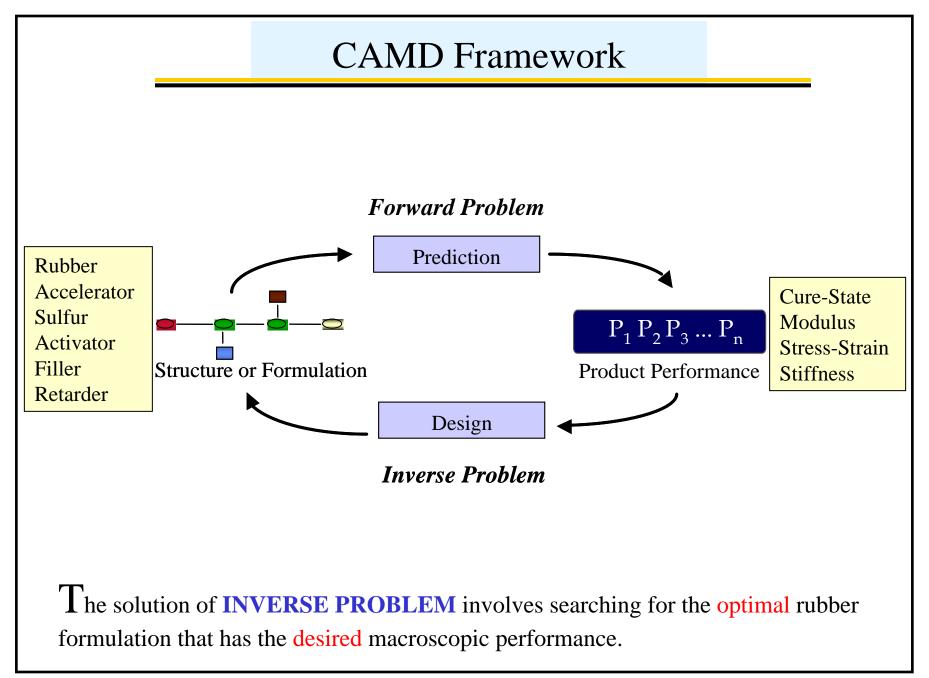


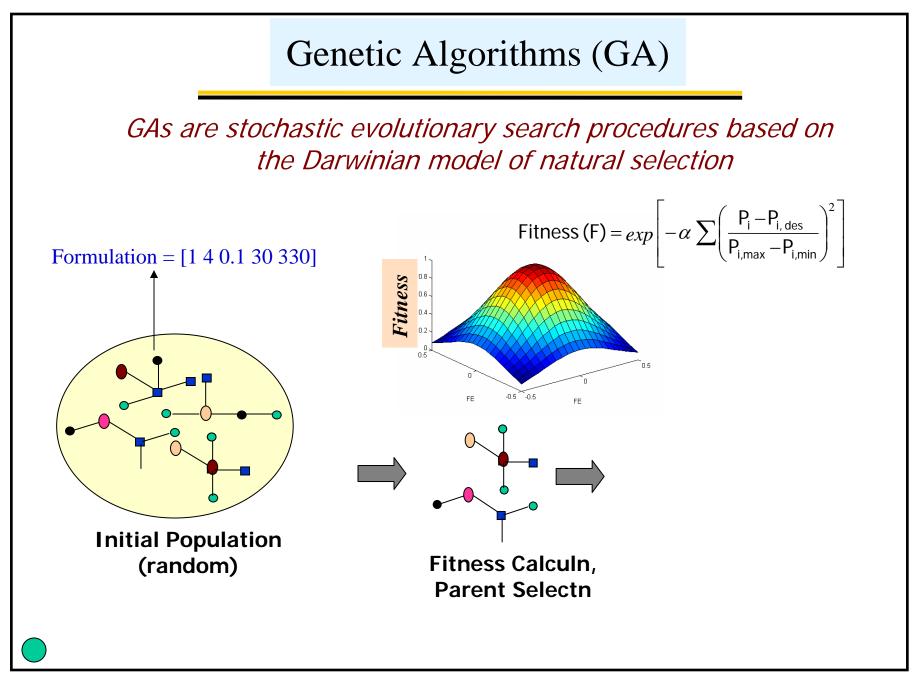
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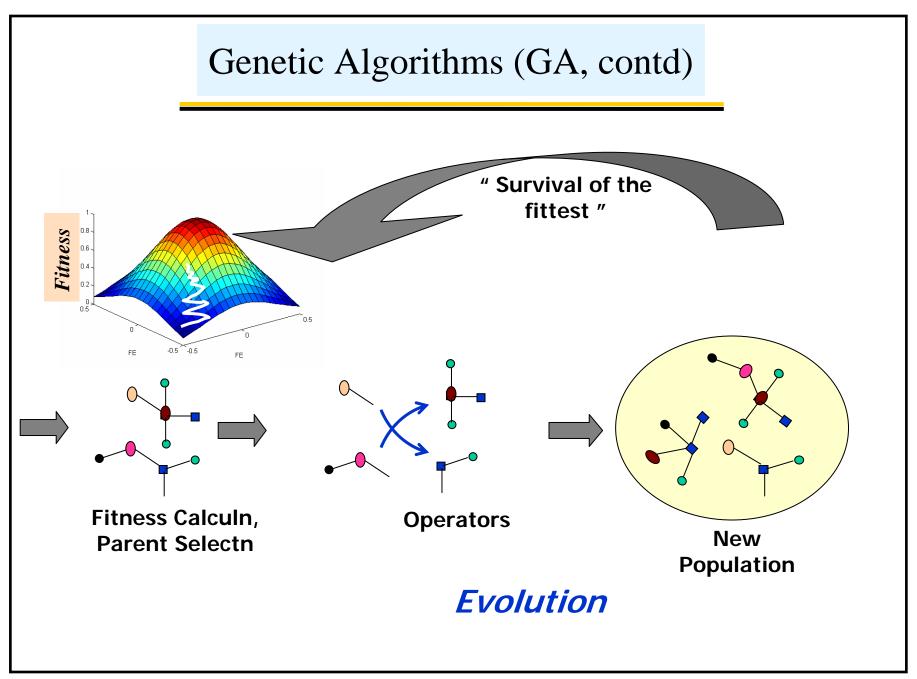


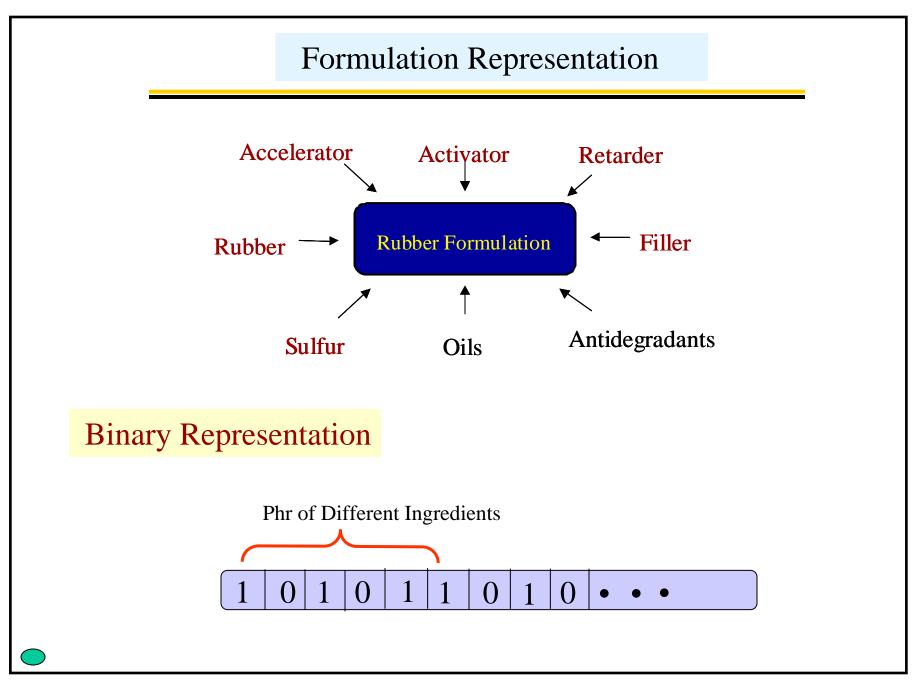


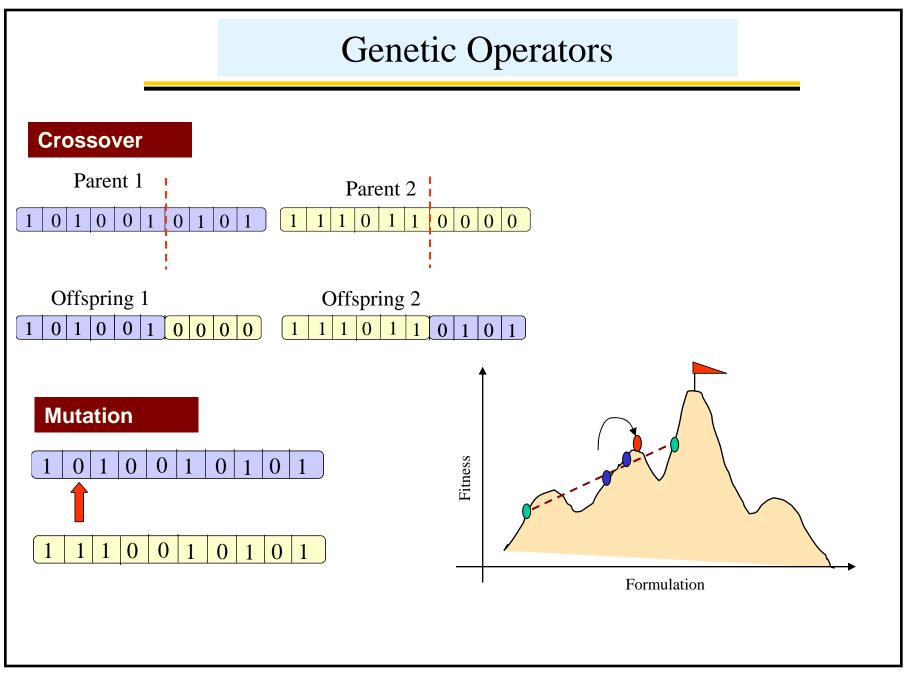
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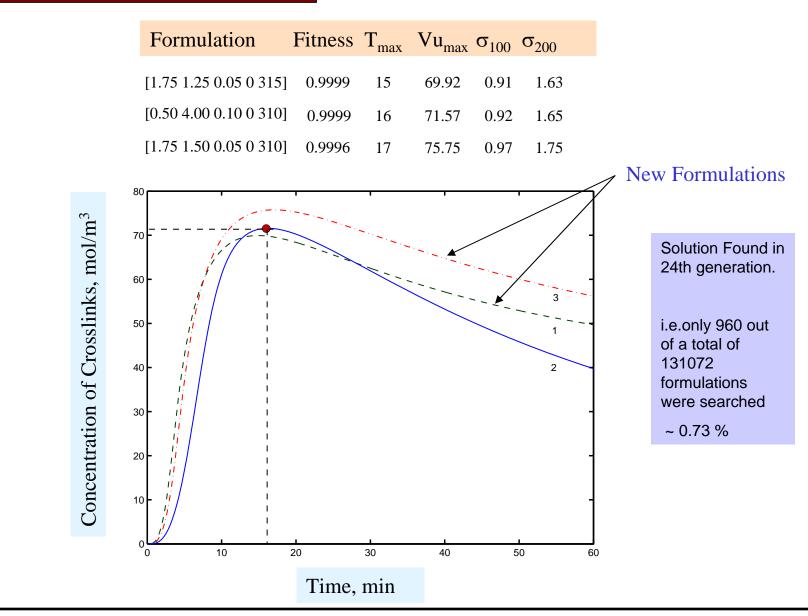
#### Inverse Problem (Results)

- Binary Representation
- Fitness Proportionate Selection
- Crossover Probability = 0.8, Mutation Probability = 0.2
- Population Size = 40, Number of Generations = 40, Elitism = 10%

Example	e 2
---------	-----

Desired Property	Optimal Formulations					
$T_{max}$ (time to reach max cure) = 16 min	Formulation	Fitness	T <sub>max</sub>	Vu <sub>max</sub>	$\sigma_{100}$	$\sigma_{200}$
$Vu_{max}$ (crosslink @ $T_{max}$ ) = 71.5 mol/m <sup>3</sup>	[1.75 1.25 0.05 0 315]	0.9999	15	69.92	0.91	1.63
	[0.50 4.00 0.10 0 310]	0.9999	16	71.57	0.92	1.65
Stress (100% Elongation) = 0.92 MPa	[1.75 1.50 0.05 0 310]	0.9996	17	75.75	0.97	1.75
Stress (200% Elongation) = 1.65 MPa	[0.75 2.75 0.10 0 315]	0.9994	13	67.88	0.88	1.58
	[3.00 0.75 0.10 0 315]	0.9991	17.5	65.34	0.85	1.52
	[2.75 1.00 0.25 0 330]	0.9990	10.5	70.46	0.93	1.67

#### BEST THREE FORMULATIONS



Interface	Caterpillar on a Daily Basis
PRAS Ver 1.1 (Purdue University)	
FORMULATION DETAILS Number 1	
ElastomerNRCarbon BlackOther AdditivesAcceleratorTypeN351ZnO4TypeMBTSComposition30PPD3Composition4DBPA129Stearic Acid2.5Sulfur1.25Ddine No.67FetarderFetarder	Plot         Image: Second
CURE CONDITIONS         Temperature       332         Time       100         Cure State (time) at         Stress Measurements         Optional	Save Output As ? X Save in: 🔄 new-software 💽 🖻 📺 📰
OUTPUT OPTION     STRESS PREDICTIONS, MPa       Both     Run   Save Plot	File name:     myoutput     Save       Save as type:     Text files (*.txt)     Cancel

## **Pharmaceutical Product Development and Engineering**



# THE WALL STREET JOURNAL.

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WEDNESDAY, SEPTEMBER 3, 2003 - VOL. CCXLII NO. 45 - \*\*\*\* \$1.00

### Factory Shift

New Prescription For Drug Makers: Update the Plants

After Years of Neglect, Industry Focuses on Manufacturing; FDA Acts as a Catalyst

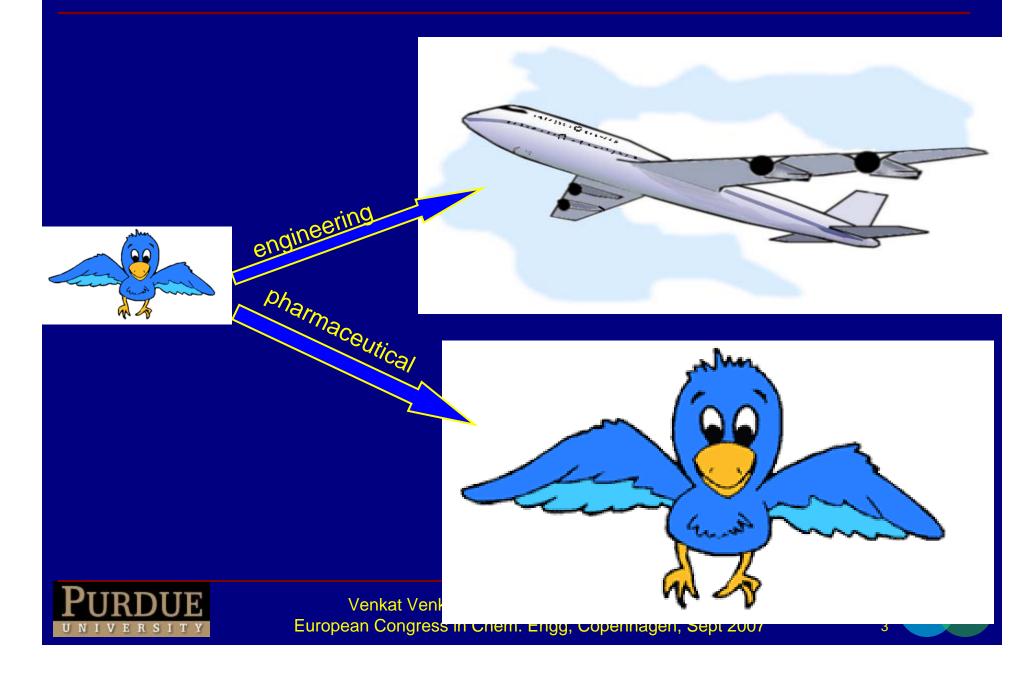
The Three-Story Blender

By LEILA ABBOUD And SCOTT HENSLEY  Prescription drug recalls • 176 in 1998 248 in 2001 354 in 2002 Schering-Plough Corp. recalled 59 million asthma inhalers in 1999 and 2000 -- unknown number were shipped empty. Semiconductor Manufacture 6 σ 5 to 5.5 σ Chemicals Pharma **2.5** σ

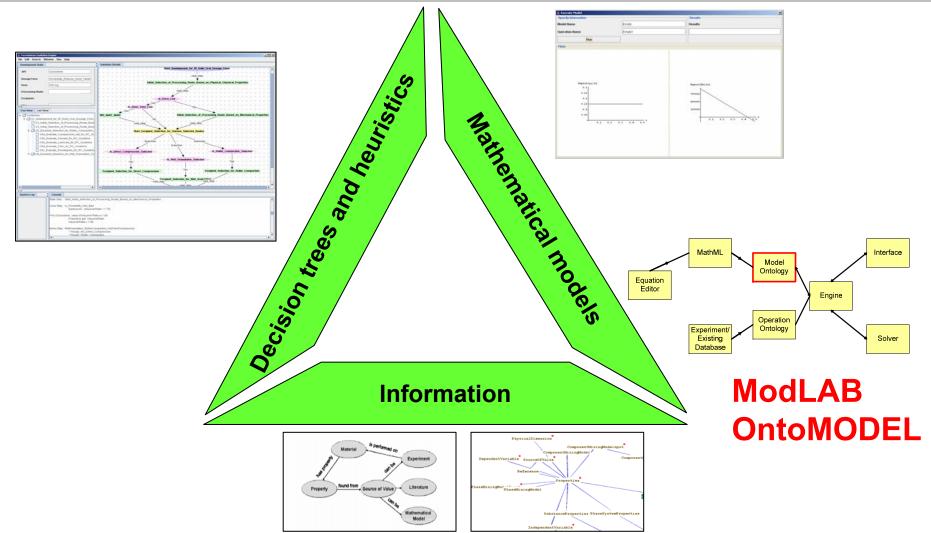
PURDUE UNIVERSITY

Venkat Venkatasubramanian, Keynote Lecture, European Congress in Chem. Engg, Copenhagen, Sept 2007 LIPS

## Pharma Industry's Scale-up Challenge



# Purdue Ontology for Pharmaceutical Engineering (**POPE**)



ENGINEERING RESEARCH CENTER FOR STRUCTURED ORGANIC PARTICULATE SYSTEMS RUTGERS UNIVERSITY PURDUE UNIVERSITY NEW JERSEY INSTITUTE OF TECHNOLOGY UNIVERSITY OF PUERTO RICO AT MAYAGUEZ



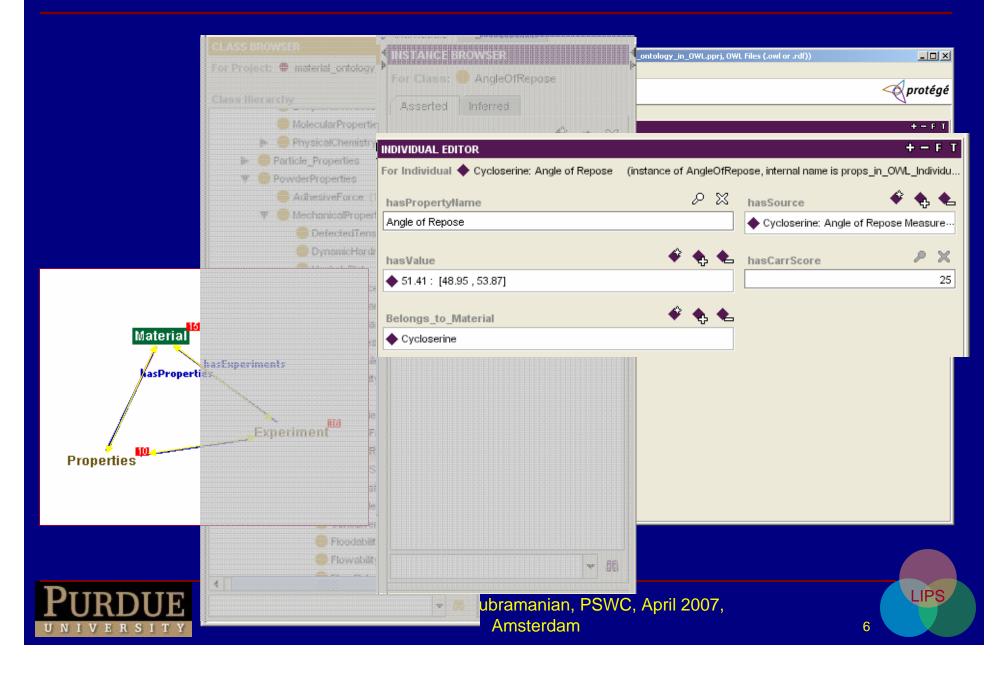
## **Ontologies Developed So Far in Our Project**

- Equipment ontology
  - Standards referenced: STEP, AP231, FIATECH
- General recipe ontology
  - RecipeElement, UnitProcedure, Operation etc.
  - Standards referenced: ISA S88, S95, OntoCAPE
- Process safety ontology
  - Deviation, Cause, Consequence etc.
- Material ontology for pharmaceutical product development
  - Flow property, Angle\_of\_Fall, Carrs\_Index etc.
- Reaction mechanism ontology
  - Molecule, Atom, Bond, Reaction etc.
  - Referenced: Chemistry Development Kit
- Model ontology
- Guideline ontology
  - Referenced: GuideLine Interchange Format

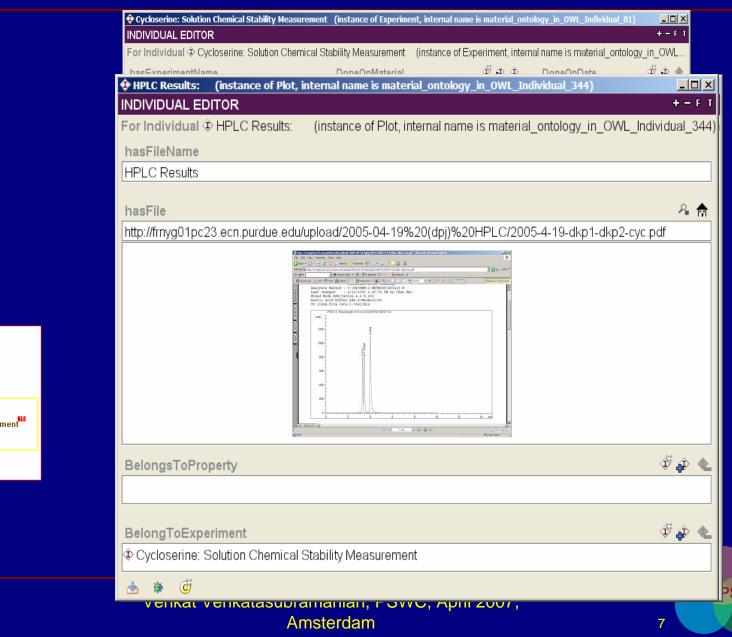


Venkat Venkatasubramanian, Keynote Lecture, European Congress in Chem. Engg, Copenhagen, Sept 2007 LIPS

## Material Property Ontology in Protégé



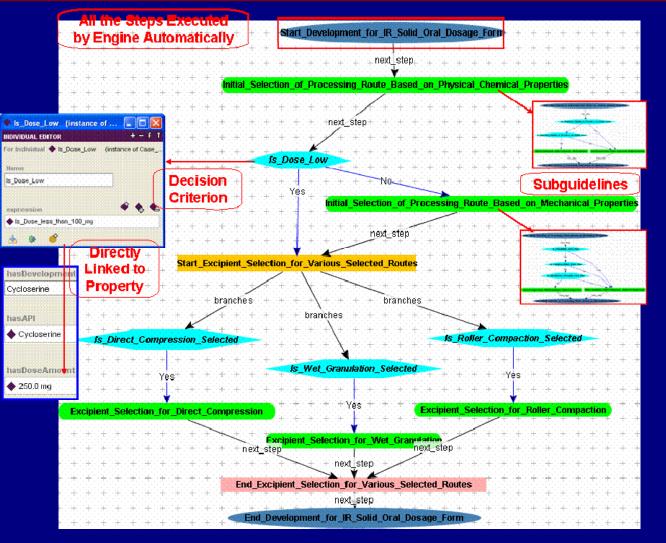
# **Experiment Ontology**





UNIVERSITY

### **Guideline Ontology for Dosage Form Formulation**



Follows GLIF (Guideline Interchange Format), A standard ontology for clinical guidelines

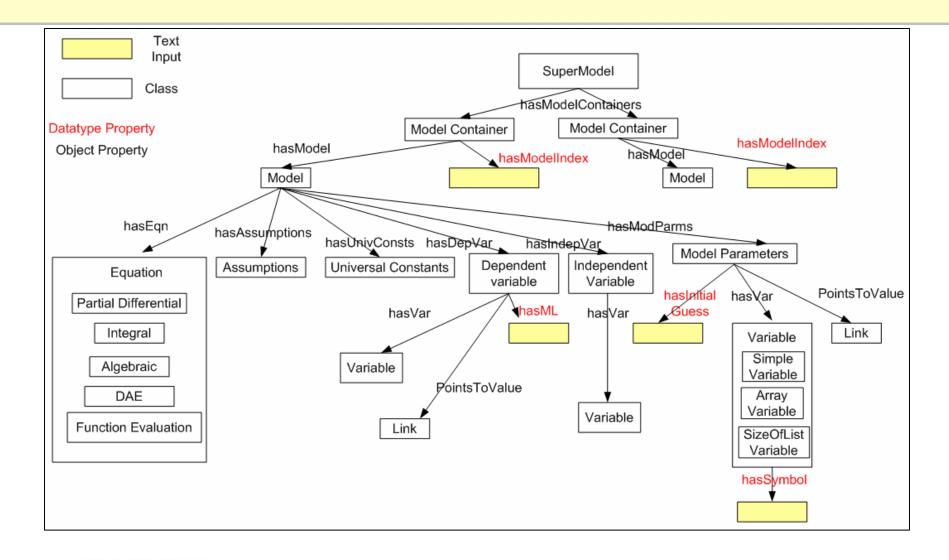


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LIPS

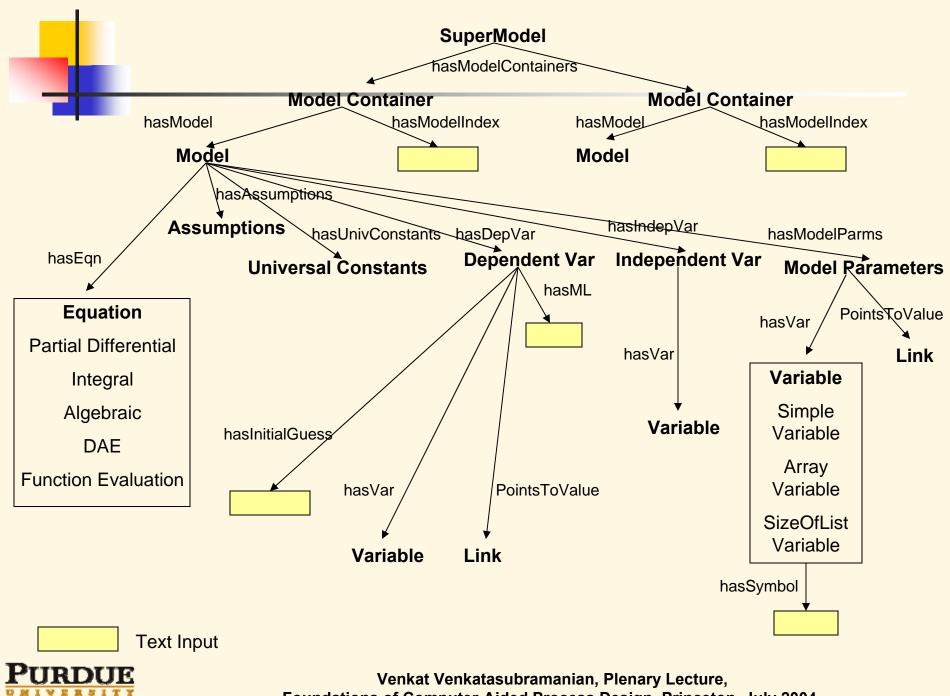
# Model Ontology



ENGINEERING RESEARCH CENTER FOR STRUCTURED ORGANIC PARTICULATE SYSTEMS

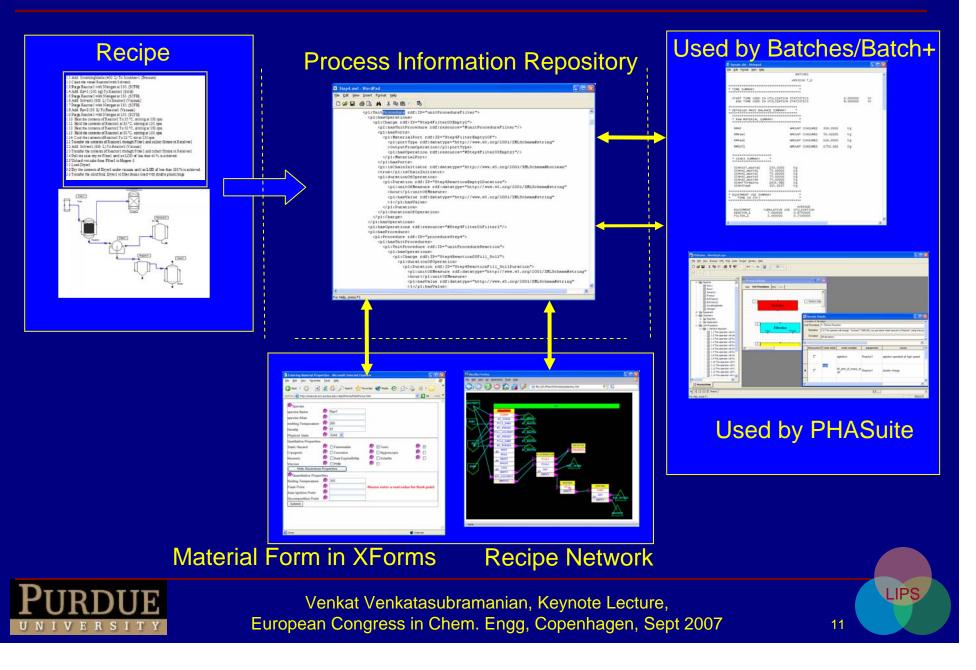
RUTGERS UNIVERSITY PURDUE UNIVERSITY NEW JERSEY INSTITUTE OF TECHNOLOGY UNIVERSITY OF PUERTO RICO AT MAYAGÜEZ



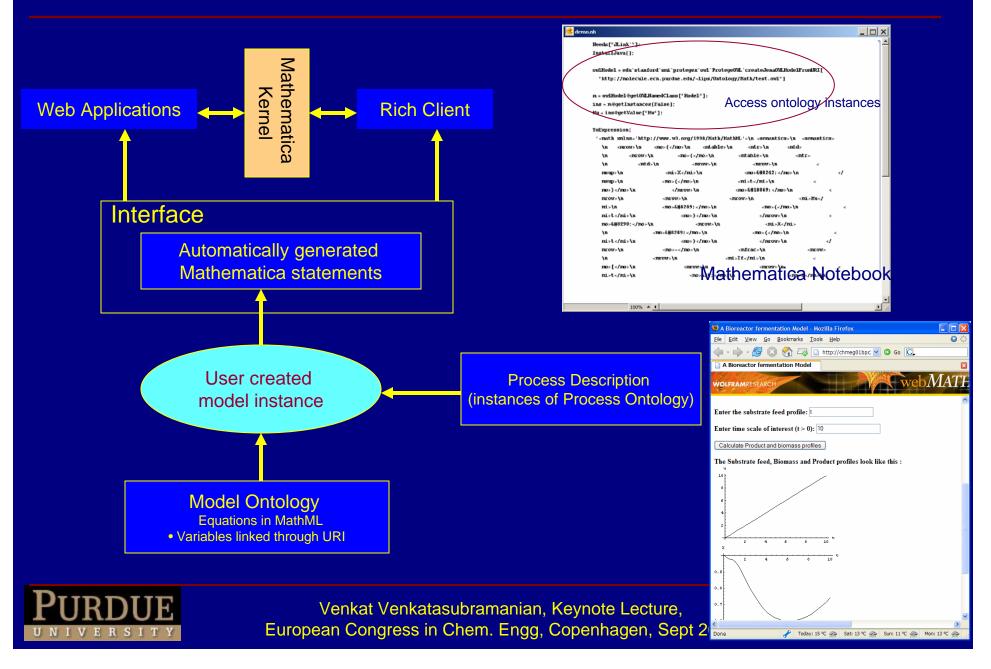


Foundations of Computer-Aided Process Design, Princeton, July 2004.

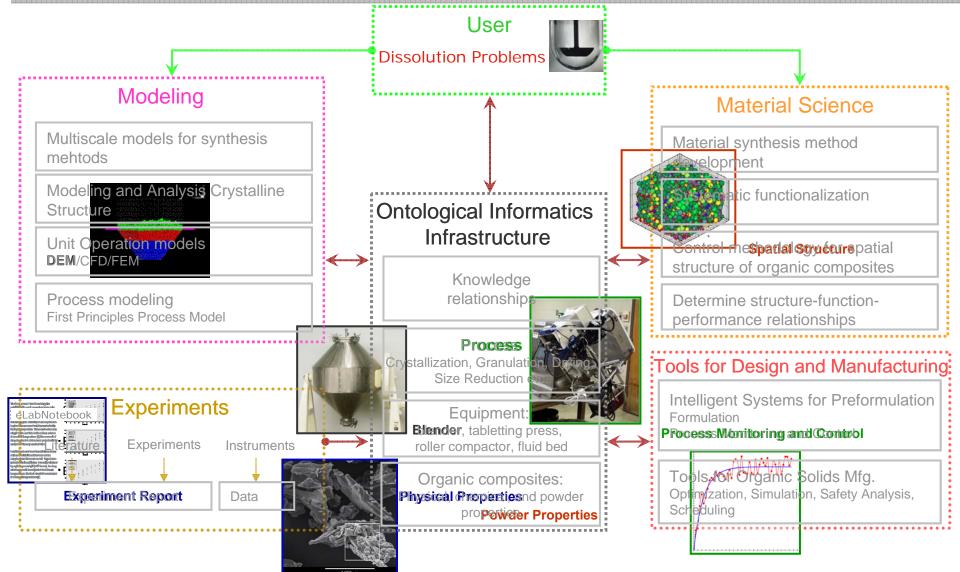
## **Integrated Model-based Decision Support**



## Integrating with Mathematical Knowledge



# Cyberinfrastructure for Real-time Decision Support for Design, Control, and Optimization



# Summary

- Reviewed Modeling and Informatics Challenges in Molecular Products Design and Engineering
- Need for Cyberinfrastructure Concepts, Methods, and Tools
- Ontological approach for information and knowledge modeling
  - Beyond ERP, SAP, Oracle, Expert Systems etc.
  - This is not just programming! Nor can it be done by CS folks alone!
- POPE: Purdue Ontology for Pharmaceutical Engineering
  - Conceptual foundation for next the generation, integrated, decision support tools environment
- This is only a beginning....Miles to go before we sleep....
- Huge opportunities for Process/Product Systems Engineers



Venkat Venkatasubramanian, Keynote Lecture, European Congress in Chem. Engg, Copenhagen, Sept 2007 LIPS

# Thank You for Your Attention!



# Any Questions?